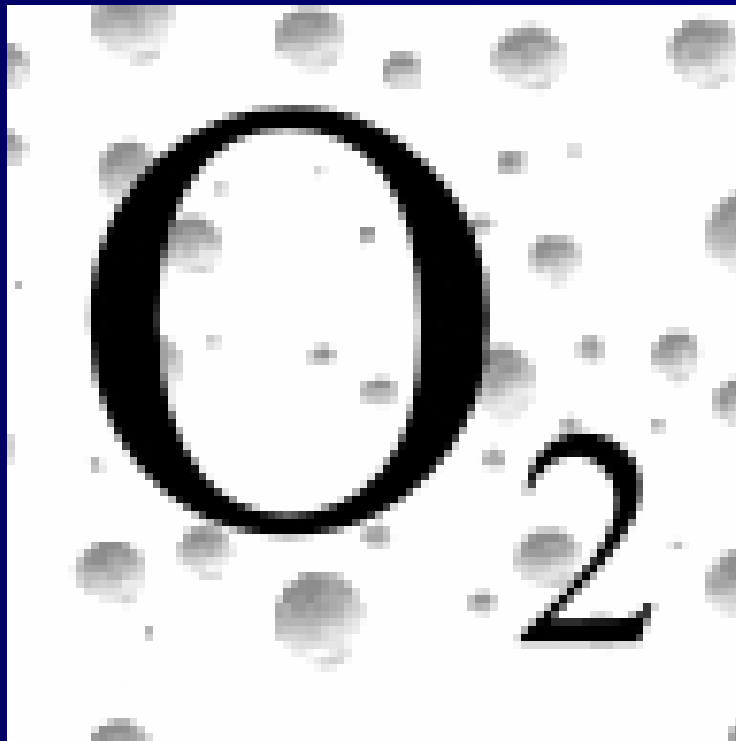


# 99% Oxygen Production with Zeolites and Pressure Swing Adsorption: Designs and Economic Analysis



Presentation by:  
**Blake Ashcraft**  
**Jennifer Swenton**

# Project Goals

- Develop a portable and hospital air separation process/device with silver zeolites to produce a continuous flow of 99% oxygen
- Recommend the application of the process/device in different markets
- Determine if process/device will be profitable in those markets

# Overview

- Market for Purified Oxygen
- Air Separation Methods
- Adsorbent Materials
- Proposed Use of Technology
- Hospital Design
- Portable Design
- Consumer Utility and Preference
- Business Plan
- Risk
- Recommendations

# Market for 99% Oxygen

- Oxygen is the third most widely used chemical in the world
- Annual worldwide market of over **\$9 billion**.

## Main applications:

- Medical oxygen for hospitals and individual use
- Industrial applications for refineries and processing plants

# Oxygen in Medicine

- Inhalation therapy
- During surgery to maintain tissue oxygenation under anesthesia
- Resuscitation of patients
- The treatment of such diseases as chronic obstructive pulmonary disease, pneumonia, and pulmonary embolism
- For the newborn experiencing respiratory distress syndrome
- The treatment of respiratory burns or poisoning by carbon monoxide and other chemical substances

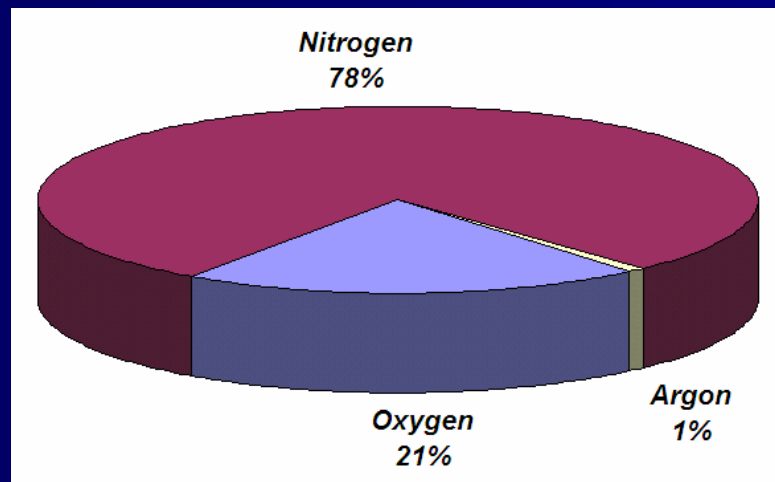
# Portable Oxygen Concentrators

- Currently no portable device capable of producing 99% oxygen continuously
- Portable oxygen cylinders with 99% oxygen lasts up to 8 hours
- Percentage of individuals suffering from lung diseases such as chronic obstructive pulmonary disease (COPD) is increasing
- COPD is 4<sup>th</sup> leading cause of death worldwide

# Hospital Unit

- Large hospitals spend an estimated \$170,000 per a year on oxygen
- Approximately 350 large hospitals in United States
- On-site unit allows for:
  - unlimited supply of Oxygen
  - Annual savings

# Air Separation



- Air is used as feed stock
- Oxygen is separated based on physical characteristics
- Must remove Nitrogen and Argon for 99% Oxygen purity



# Air Separation Methods

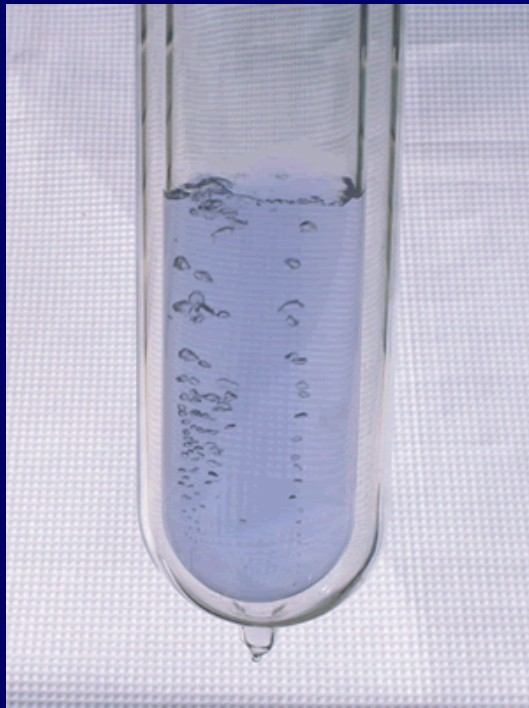
- Cryogenic Distillation
- Membrane Separation
- Pressure Swing Adsorption (PSA)



# Cryogenic Separation



# Cryogenic Separation



- Leading process for producing 99% oxygen in bulk.
- Involves liquidifying air and distilling the liquid air to separate the Oxygen, Nitrogen, and Argon.
- Can be sold in a liquid form.  
1 L of liquid Oxygen = 860 L of gaseous Oxygen

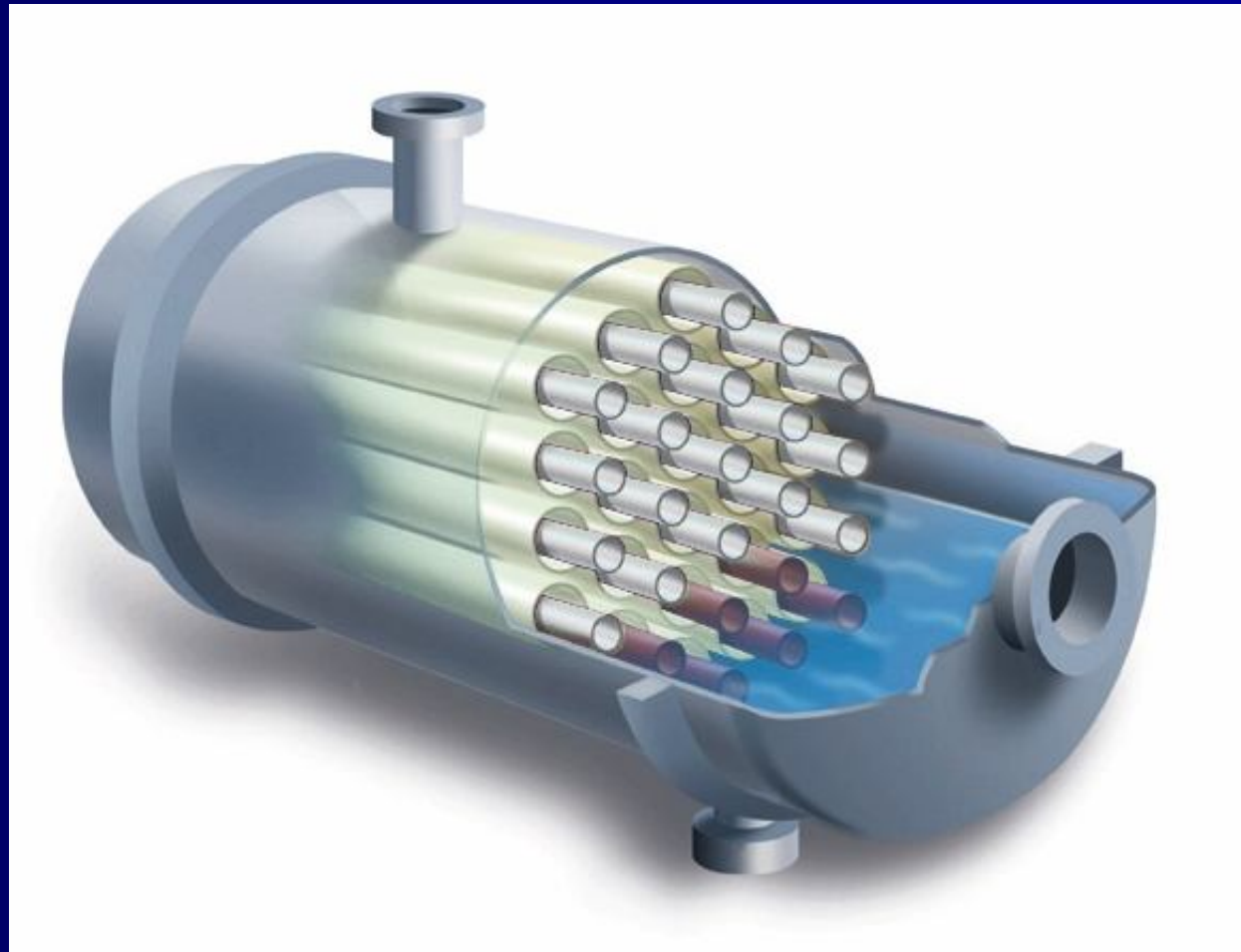
# Cryogenic Separation

## ■ Drawbacks

- Process uses large bulky equipment
- Energy requirements are substantial unless demand is more than 60 tons of oxygen per a day
- Liquid oxygen evaporates back into the atmosphere over time

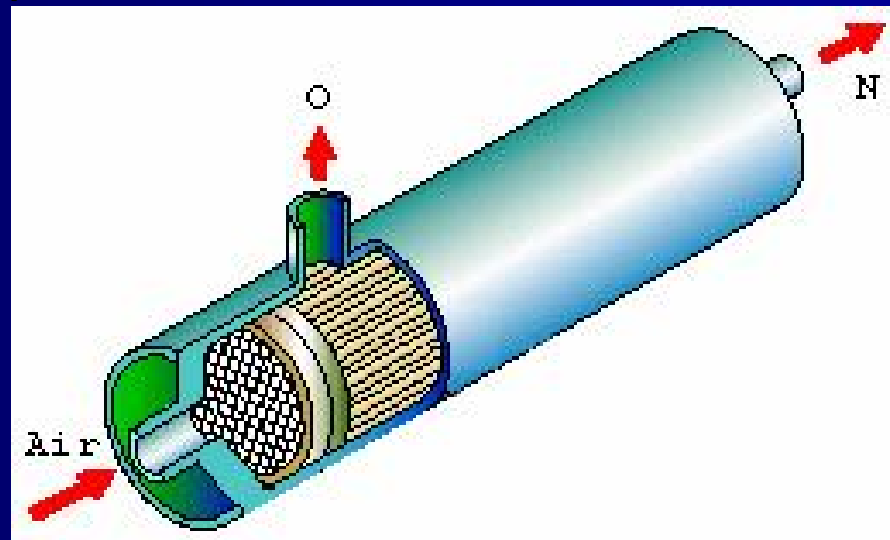


# Membranes



# Membranes

- Permeable materials used to selectively separate Oxygen, Nitrogen, and Argon
- Large and medium scale production.
- Pressurized air is passed through the membrane and is separated by permeability characteristics of each component in relation to the membrane.



# Membranes

## Drawbacks

- Membranes require a large surface area to achieve high product flow rates.
- Large pressures are typically used
  - Safety hazard
  - Large compressors
- Oxygen and Argon molecules are similar in size and have similar permeability properties.
  - This results in a selectivity of  $\approx 2.5$  O<sub>2</sub>/Ar and a low oxygen recovery.

# Pressure Swing Adsorption





# Pressure Swing Adsorption

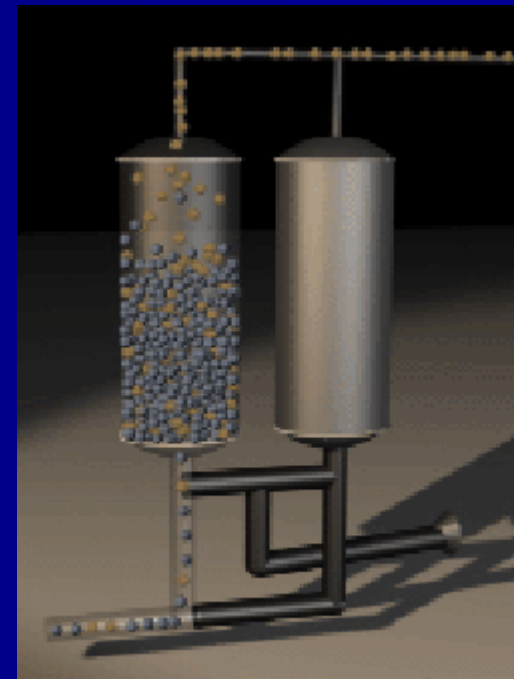
- Uses sorbents (zeolites, nanotubes) in two adsorption columns to separate molecules.
- Two columns allow for the process to operate semi-continuously.
- 4 Process stages
  - Adsorption/Production
  - Blowdown/Purge



# Pressure Swing Adsorption

## *Stage 1*

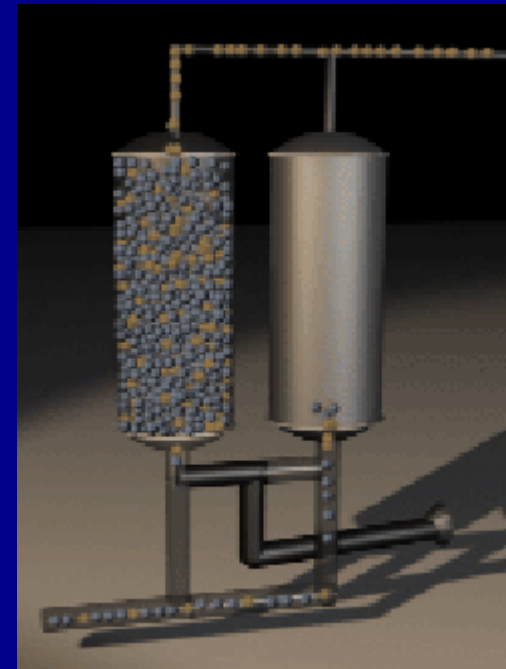
- Compressed air is fed into the first bed.
- Nitrogen and argon molecules are trapped, while oxygen is allowed to flow through.



# Pressure Swing Adsorption

## *Stage 2*

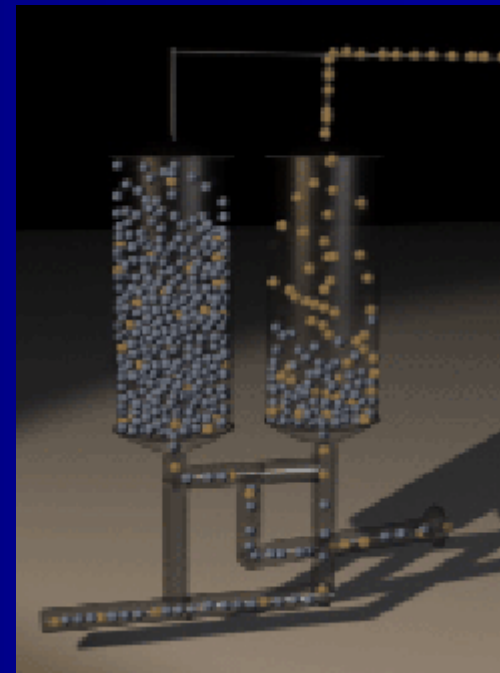
- The adsorbent in the first bed becomes saturated with nitrogen and argon molecules
- The airflow feed is directed into the second bed.



# Pressure Swing Adsorption

## *Stage 3*

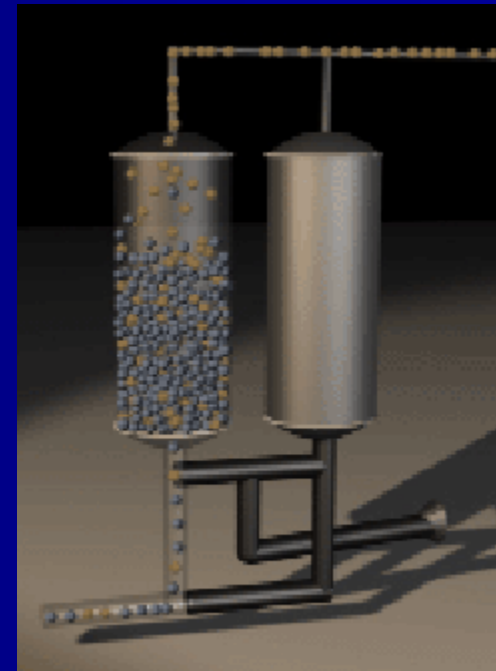
- The adsorbent adsorbs nitrogen and argon in the second bed.
- The first bed is depressurized allowing argon and nitrogen to be purged out of the system and released to the atmosphere.



# Pressure Swing Adsorption

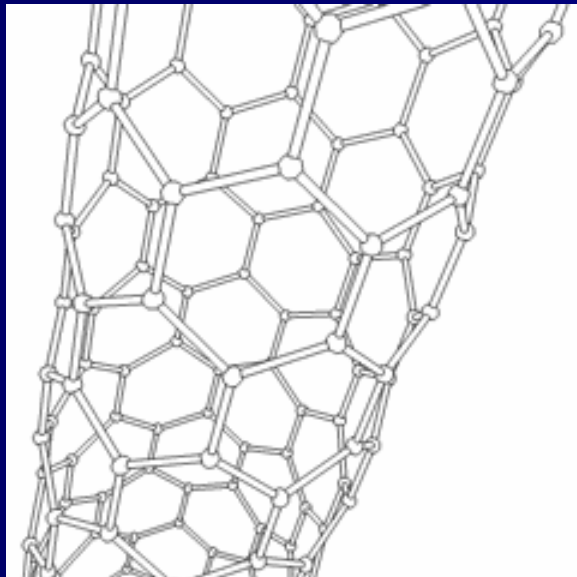
## *Stage 4*

- The process starts over.
- Compressed air is once again fed into the first bed.
- The second bed is depressurized releasing argon and nitrogen molecules to the atmosphere.



# Adsorbents for PSA

- Introduction to Zeolites and Carbon Nanotubes
- Structures
- Applications



# Silica Gel Pretreatment

- Pretreatment bed to remove water vapor and impurities such as carbon dioxide
  - Air at 100% humidity is approximately 3% water vapor
- Water can impair the performance of adsorbents in the PSA adsorption columns.
- Silica gel beds are necessary to remove water vapor from the air.
  - A heating coil used to evaporate the water from the silica gel

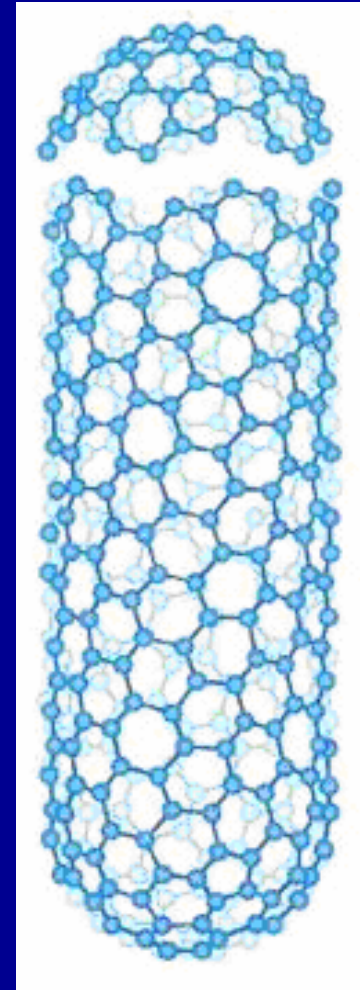
# Kinetic Separation

- Molecular Sieve Carbon (MSC) adsorbents using PSA technology
- Ideal for separation of Argon and Oxygen
  - MSCs in kinetic adsorption can adsorb Oxygen 30 times faster than Argon
    - Creates a problem in design, requiring two PSA systems to collect the adsorbed Oxygen



# Carbon Nanotubes

- Sheets of carbon atoms rolled into tubes of varying diameters
- Nanotubes have extraordinary strength
- Potential uses in many industrial processes, including adsorption.



# Carbon Nanotubes

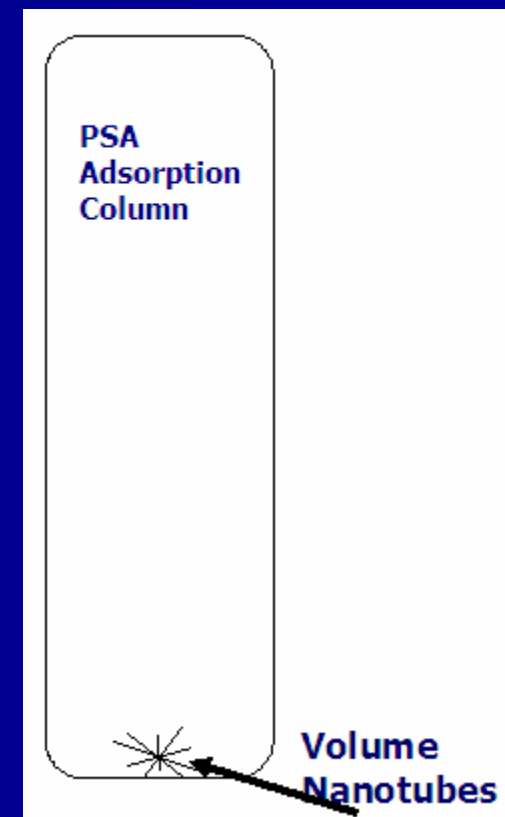
## Advantages

- Nanotubes have little interaction with nitrogen at high temperatures due to oxygen's higher packing efficiency, smaller diameter, and entropic energies
- Research has shown that single walled carbon nanotubes (SWCN) of 12.53Å have a selectivity of O<sub>2</sub>/N<sub>2</sub> of 100:1 at 10 bar.
- It has been indicated that Argon will have very little interaction with nanotubes

# Carbon Nanotubes

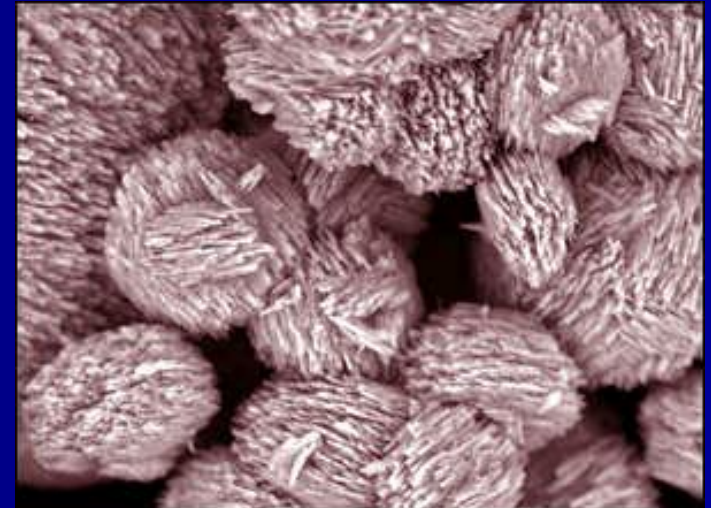
## Disadvantages

- Nanotubes are so efficient the volume of nanotubes required for separation of air is much smaller than the volume of feed air.
  - Nanotubes' surface area is not large enough to react with the volume of air required.
  - No current way to disperse nanotubes effectively for PSA air separation
- Price range for nanotubes is \$325 to \$500 per gram



# Zeolites

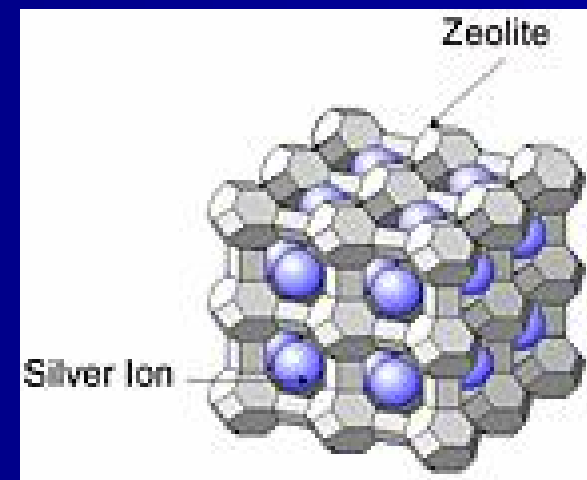
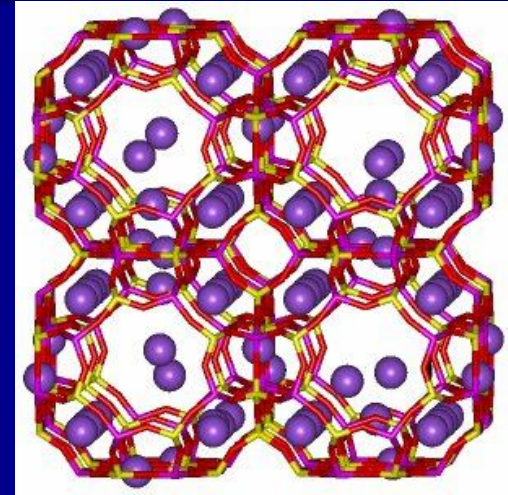
- Microporous crystalline structures
- Lifespan of 10 years
- The zeolite's structure governs which molecules are adsorbed.
- Various ways of controlling adsorption
  - separate molecules based on differences of size, shape and polarity



# Zeolites

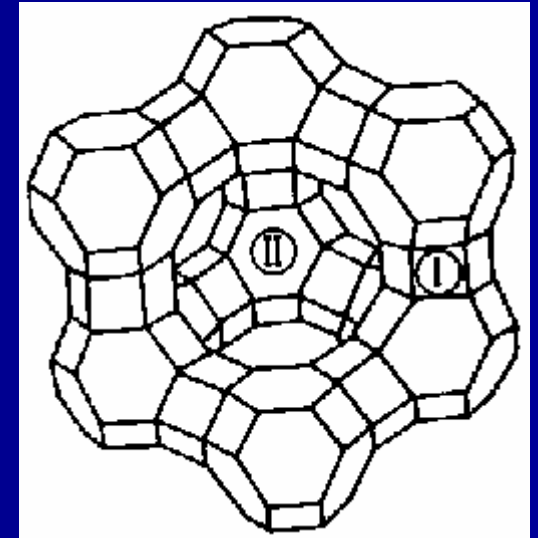
## Ion Exchange:

- Metal cations (calcium, sodium, silver) are bound to the zeolite structure
  - Silver cation zeolites have been proven to be best for air separation
- Creates an electrostatic interaction between the cation ion and the molecules being adsorbed



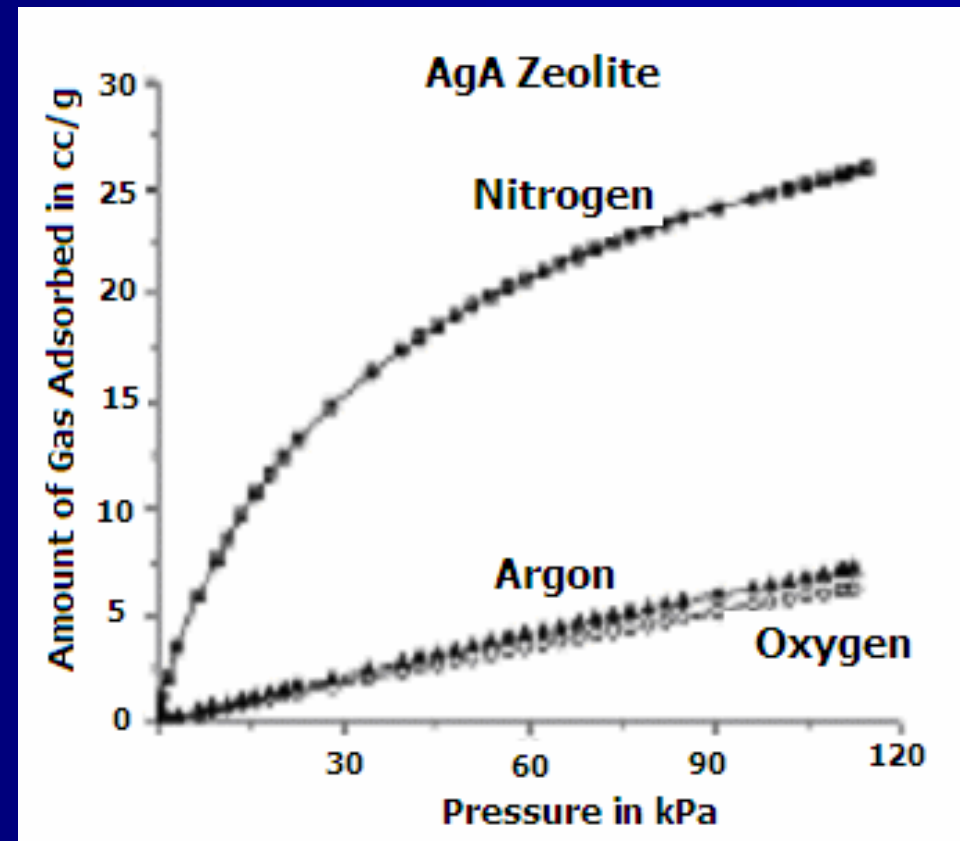
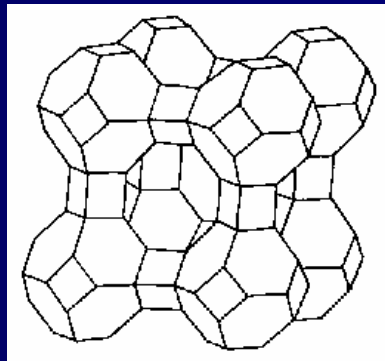
# LiAgX Zeolite

- Useful for removing Nitrogen from Oxygen with product throughput .1 kg O<sub>2</sub>/hr/kg adsorbent.
- Can obtain 96.42% oxygen purity with 62.74% Oxygen recovery.
- Drawback is the selectivity of Argon to Oxygen is approximately 1:1.



# AgA Zeolite

- Argon to Oxygen selectivity of 1.63 to 1
- 7 cm<sup>3</sup>/g of Argon adsorbed at atmospheric pressure
- Nitrogen to Oxygen selectivity of 5 to 1



$$F_{N_2}^0 \Delta t = \Delta L_1 A N_{N_2}^1 = v_1 A N_{N_2}^1$$

# Equilibrium Adsorption Theory

- Competition between the different molecules on the adsorbent sites exists.
  - Langmuirian Multi-component Theory is used to determine the fractional loading of each component on the adsorbent
- Selectivity describes how selective one component is to bind to the adsorbent over another component

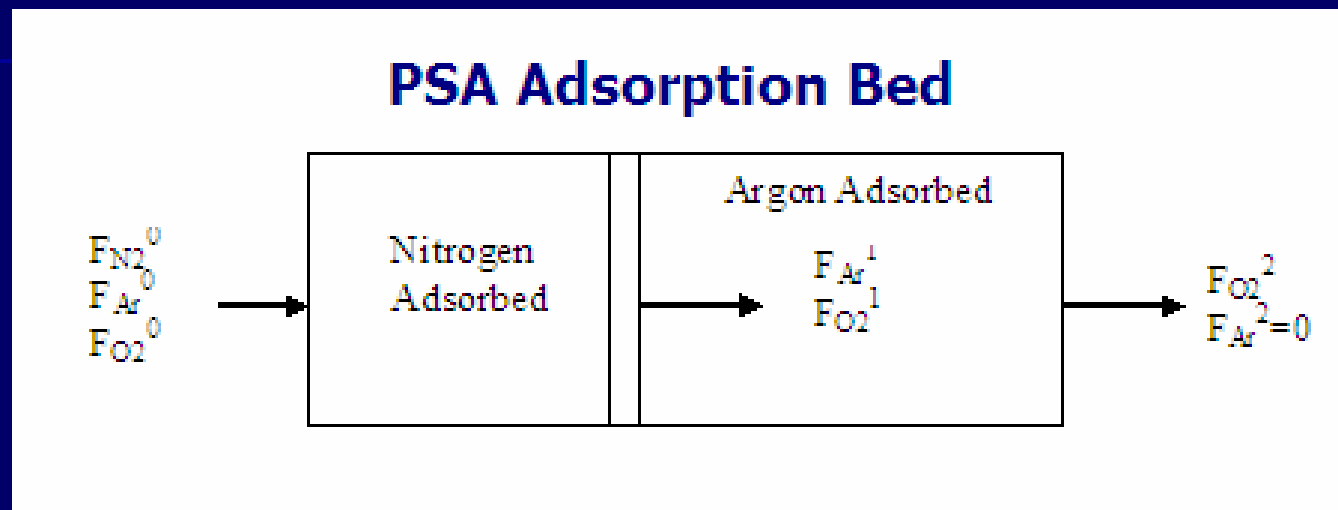
$$\theta_i = \frac{b_i P_i}{1 + \sum_{j=1} b_j P_j}$$

$$S_{ij} = \frac{b_i}{b_j}$$



$$F_{N_2}^0 \Delta t = \Delta L_1 A N_{N_2}^1 = v_1 A N_{N_2}^1$$

# Equilibrium Adsorption Theory



## ■ Material Balances

– Nitrogen  $\rightarrow F_{N_2}^0 \Delta t = \Delta L_1 A N_{N_2}^1 = v_1 A N_{N_2}^1$

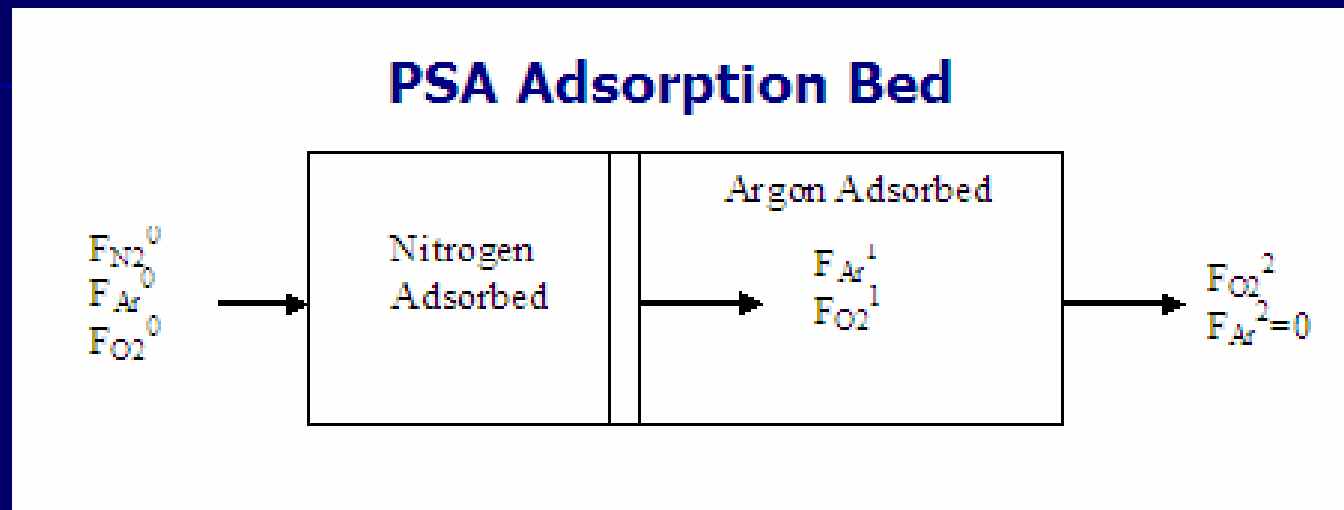
– Oxygen  $\rightarrow F_{O_2}^1 = F_{O_2}^0 + (N_{O_2}^2 - N_{O_2}^1) A v_1$

– Argon  $\rightarrow F_{Ar}^1 = F_{Ar}^0 + (N_{Ar}^2 - N_{Ar}^1) A v_1$

$\rightarrow F_{Ar}^2 = 0 = F_{Ar}^1 + N_{Ar}^2 A v_2$

$$F_{N_2}^0 \Delta t = \Delta L_1 A N_{N_2}^1 = v_1 A N_{N_2}^1$$

# Equilibrium Adsorption Theory



For the adsorption bed to remove both Nitrogen and Argon the velocity ratio of the argon front must be greater than that of the nitrogen front

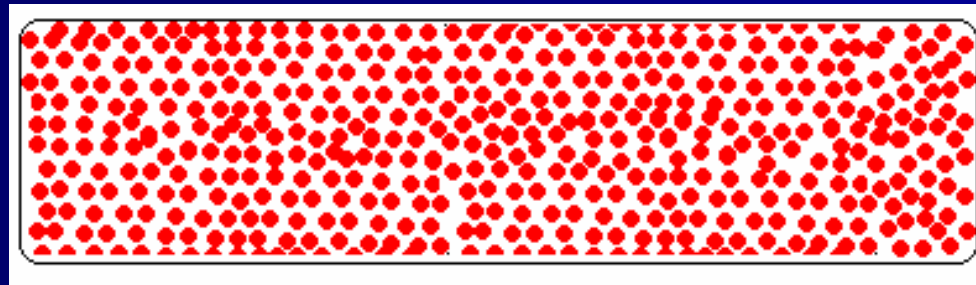
$$\frac{v_2}{v_1} = \frac{\frac{F_{Ar}^0}{F_{N_2}^0} + (N_{Ar}^2 - N_{Ar}^1)}{N_{Ar}^2} > 1$$

# **Proposed Use of the Presented Technologies**

# Proposed Use of Technology

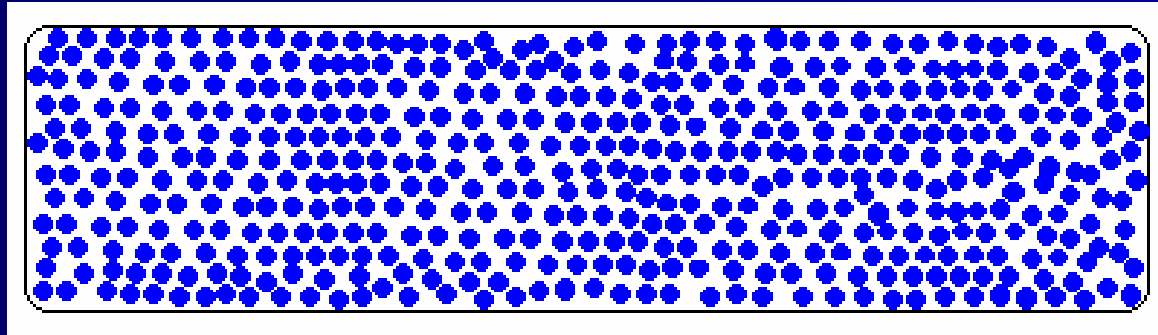
- Pressure Swing Adsorption (PSA) will be used in the design for:
  - Medium scale capacity
  - Safety
  - Cost savings
  
- An analysis of 4 designs using zeolites LiAgX and AgA in the PSA adsorption beds was performed. The column diameter and cycle time was held constant.
  - Design 1
    - LiAgX zeolite
  - Design 2:
    - AgA zeolite
  - Design 3:
    - Mixed ratio of zeolites LiAgX and AgA
  - Design 4:
    - Both LiAgX and AgA zeolites separating them

# Design 1: LiAgX zeolite



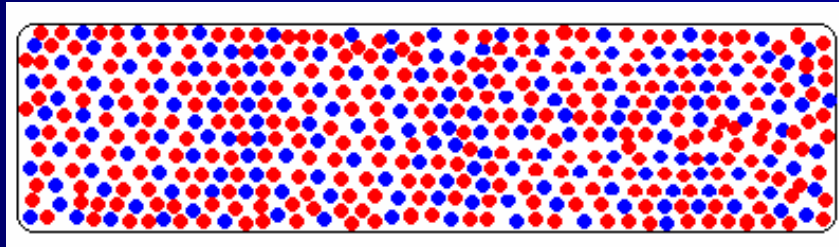
- Nitrogen Removal
  - LiAgX removes nitrogen with a 96.42% purity Oxygen and 62.74% recovery.
  - This is the best zeolite for nitrogen removal
- Argon Removal
  - Argon to Oxygen selectivity of 1:1.
  - Requires a large volume of LiAgX zeolite to accomplish required purity
- Large volume of zeolite is required. Costs and inlet airflow rate increases.

# Design 2: AgA zeolite



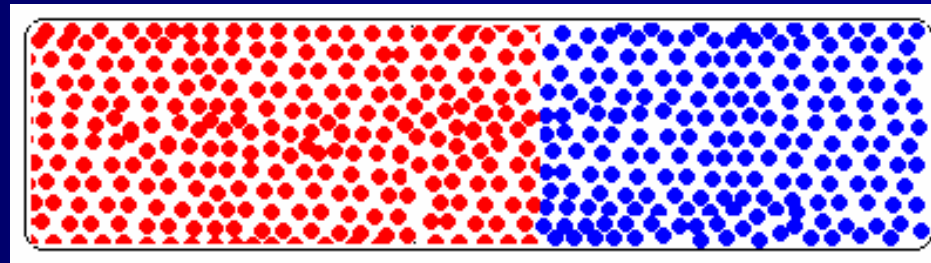
- Nitrogen Removal
  - Nitrogen to Oxygen selectivity of 5 to 1 in AgA zeolite
  - Selectivity is lower than if using LiAgX zeolite
- Argon Removal
  - Argon to Oxygen selectivity of 1.63 to 1
  - Best design for Argon removal
- Large volume of zeolite is required
  - Costs and inlet airflow rate increases.

# Design 3: Mixed zeolites



- Nitrogen Removal
  - LiAgX has a higher loading and selectivity of nitrogen than AgA.
  - Not beneficial to mix them in order to rid of the nitrogen.
- Argon Removal
  - AgA has a higher loading and selectivity toward argon, selectivity being 1.63 than LiAgX which has a 1:1 ratio
  - Mixing in LiAgX in the argon removal section would only hurt performance as well.

# Design 4: LiAgX and AgA zeolites separated

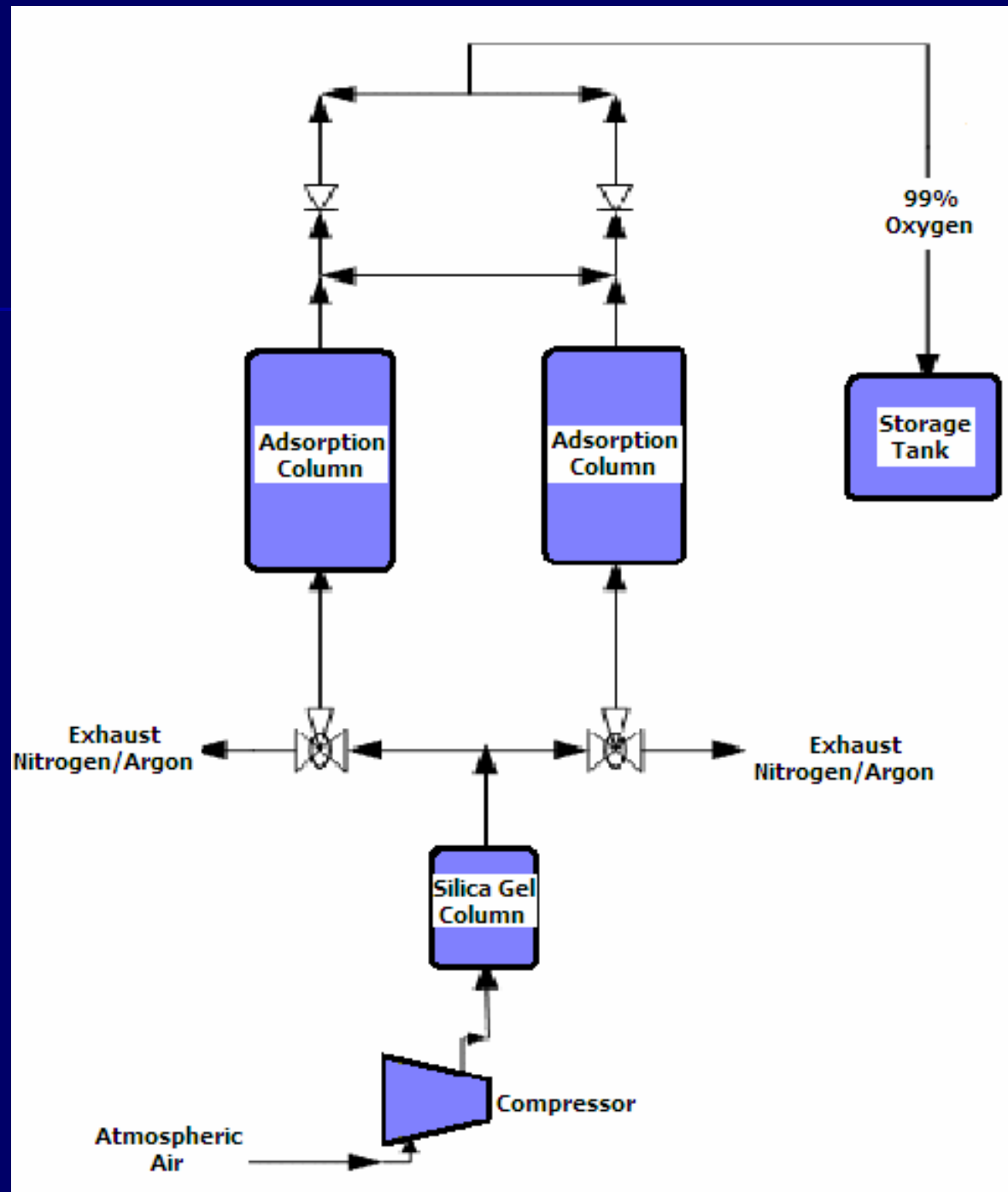


- Nitrogen
  - LiAgX zeolite with a 96.42% Oxygen purity and 62.74% recovery
- Argon
  - AgA zeolite with an Argon to Oxygen selectivity of 1.63 to 1
- The volume is dramatically lower
  - Save money on the zeolite cost and overall unit
- The inlet air flow rate would be less due to the higher recovery of oxygen
- Has been determined **most** beneficial design



# Zeolite Design Analysis

Column, Zeolite, and Flow Specifications for PSA Designs			
LiAgX Only		AgA Only	
Recovery of Inlet Oxygen	27	Recovery of Inlet Oxygen	20
Inlet Flow Rate (L/s)	1,007	Inlet Flow Rate (L/s)	1,325
Mass of LiAgX Zeolites (kg)	4,342	Mass of LiAgX Zeolites (kg)	5,714
Volume Column (cm <sup>3</sup> )	4,058,324	Volume Column (cm <sup>3</sup> )	5,339,900
Area Column (cm <sup>2</sup> )	5,027	Area Column (cm <sup>2</sup> )	5,027
Length Column (cm)	807	Length Column (cm)	1,062
50/50 Mixture		LiAgX/AgA	
Recovery of Inlet Oxygen	25	Recovery of Inlet Oxygen	35
Inlet Flow Rate (L/s)	1,060	Inlet Flow Rate (L/s)	362
Mass of LiAgX Zeolites (kg)	2,286	Mass of LiAgX Zeolites (kg)	1,614
Mass of AgA Zeolites (kg)	2,286	Mass of AgA Zeolites (kg)	601
Volume Column (cm <sup>3</sup> )	4,271,920	Volume Column (cm <sup>3</sup> )	2,069,402
Area Column (cm <sup>2</sup> )	5,027	Area Column (cm <sup>2</sup> )	5,027
Length Column (cm)	850	Length Column (cm)	412



# Hospital Air Separation Design with Pressure Swing Adsorption



# Proposed Design - Hospital

## Large hospital information

- Approximately 350 large hospitals in the United States (500-1000 beds).
- At any time have 150 users using 5L/min.



# Proposed Design - Hospital

## ■ Goals

- Use PSA technology to produce 99% oxygen with all specifications.
- Provide for maximum capacity of 300 users at 5 L/min of oxygen to adjust for fluctuation in demands.
- Determine if product is profitable and a plausible option for large hospitals.



# Proposed Design - Hospital

First calculate inlet air flow rate of air:

<b>Calculation of Inlet Flow Rate</b>	
Recovery of Oxygen (LiAgX) (%)	62.7
Recovery of Oxygen (AgA) (%)	55.0
Total Recovery of Oxygen (%)	34.5
<b>Assume 30 second Cycle Time</b>	
Outlet Oxygen needed for 300 users at 5L/min	1500
Oxygen Adsorbed per 2 columns (L)	2850
Inlet Oxygen (L/min)	4350
Inlet Air Mixture (L/min)	21750

# Proposed Design - Hospital

## Adsorbent Results

Inlet Air Mixture (L)	21750.0
Inlet Air Feed to each column (L)	10875.0
Flow rate air to each column (L/s)	362.5
LiAgX Section of Column	
Product Throughput kg O <sub>2</sub> /h/kg adsorbent	0.1
Total 96.42% Pure Oxygen from LiAgX	2729.2
Mass of LiAgX Zeolites (kg)	3303.0
AgA Section of Column	
Total Entering O <sub>2</sub> /Ar mixture (L)	1447.8
Product Throughput kg O <sub>2</sub> /h/kg adsorbent	0.2
Mass of AgA Zeolites (kg)	1229.5

# Proposed Design - Hospital

## Column Specifications

Total Mass of Zeolites per Column (kg)	4532
Total Volume of Zeolites per Column (L)	4236

## Column Data

Volume of Column (L)	4236
Diameter of Column (cm)	80
Height of Column (cm)	421
Total Loading of N <sub>2</sub> /O <sub>2</sub> /Ar per Column (kg)	22



# Proposed Design - Hospital

## Final Components of Design

### Compressor (Palatek)

Max Flow of Compressor (CFM)	900
Inlet Flow to be Compressed (CFM)	776
Power Consumption (hP)	200

### Silica Gel Drying Column

Volume (cm <sup>3</sup> )	20291
Height (cm)	65
Diameter (cm)	20
Mass of Silica Gel (kg)	12

# Proposed Design - Hospital

## Components Continued

### High Pressure Storage Tank

Volume to be stored in 60 minutes (L)	92100
Volume of stored air at 10 atm	9210

### Compressor for High Pressure Storage (Palatek)

Inlet Flow to be Compressed (CFM)	55
Max Flow of Compressor (CFM)	100
Power Consumption (hP)	50

# Proposed Design - Hospital

<b>Important Results</b>	
Purity of Air (LiAgX)	96.42
Volume of O <sub>2</sub> /Ar out of LiAgX Section	1448
<b>Purity of Air (AgA)</b>	<b>&gt;99</b>
Vol. 99% Oxygen out of 1 Column/30 sec	750
Volume 99% O <sub>2</sub> out in 1 min	1501
<b>Users Supplied at 5L/min</b>	<b>300</b>

## Goals met:

Producing 99% Oxygen

Supply 300 users of oxygen at 5L/min!

# Portable Oxygen Concentrator Design



# Portable Oxygen Concentrators

## Market Designs:

- Only alternative to carrying bottles of oxygen.
- Uses PSA to purify air stream.
- Small enough to carry. Less than 30 lbs.
- Uses battery power to increase portability.
- 85%-95% oxygen purity.



# Portable Oxygen Concentrators

## Necessary Requirements

1. Weighs less than 30 lbs.
2. 99% oxygen purity at 5 liters per minute.
3. Battery life of at least 8 hours.
4. Small enough to take on airplane
5. Low noise
6. Less than \$5,000/unit and covered by medicare.

<b>Oxygen Concentrator</b>				
		Weight		
<b>Parts</b>	<b>#</b>	<b>kg</b>	<b>Price</b>	<b>Cost</b>
<i>Column and Tanks</i>				
Adsorption Columns (Al) 1.5 liter	2	1.86	\$100.00	\$200.00
Drying Column (Al) 1 liter	1	0.0115	\$100.00	\$100.00
Low Pressure Storage tank (Al) 2 liter	1	1.86	\$100.00	\$50.00
<i>Packing</i>				
LiAgX Zeolites (Adsorbent)		5	\$.4/g	\$2,000.00
Silver Zeolite A (Adsorbent)		1.4	\$.4/g	\$560.00
Silica Gel (Drying)		0.08	\$.05/g	\$4.00
<b>Other items</b>				
Inlet Feed Compressor	1	2.73	\$100.00	\$100.00
Nitrogen Exhaust Muffler	1	0.23	\$3.00	\$3.00
3 Way Ball Valve	2	0.09	\$100.00	\$200.00
2 Way Solenoid Valve	2	0.09	\$100.00	\$200.00
Battery	3	0.93	\$100.00	\$300.00
Control Computer	1	0.09	\$300.00	\$300.00
Frame (Aluminum)	1	0.91	\$100.00	\$100.00
Casing (Plastic)	1	0.09	\$75.00	\$75.00
<b>Final Total Weight (kg)</b>		<b>9.35</b>	<b>Total Cost =</b>	<b>\$4,192.00</b>
<b>Final Total Weight (lb)</b>		<b>20.57</b>		

# Portable Oxygen Concentrators

Goals met with portable oxygen concentrator from initial estimates:

**Purity:** 99% Oxygen

**Cost:** \$4200 under \$5000

**Weight:** 20.5 lb under 30lb

**Small:** Estimated Volume .6ft x 1ft x 1ft



# Portable Oxygen Concentrators



# Portable Oxygen Concentrators

## Conclusions/Recommendations:

A competitive/lightweight portable oxygen concentrator with 99% oxygen can be produced.

Perform extensive design estimates and economic analysis.

# Consumer Utility and Preference



# Consumer Utility and Preference

- Method used to determine relationship between:
  - consumer preference
  - satisfaction

in order to predict product price and product demand.



# Consumer Utility and Preference

## Theory

The solution to consumer utility maximization is given by:

$$\phi(d_1) = p_1 d_1 - \left(\frac{\alpha}{\beta}\right)^\rho p_2 \left[\frac{Y - p_1 d_1}{p_2}\right]^{1-\rho} d_1^\rho = 0$$

$\alpha$  = Inferiority Function (Knowledge of product, function of time)

$\beta$  = Superiority Function (Consumer preference, comparison to competition "preference")

$Y$  = Consumer budget =  $p_1 * d_1 + p_2 * d_2$

# Consumer Utility and Preference

- Further Quantification of  $\beta$   
(ratio of consumer preference)

$$\beta = \frac{H_2}{H_1}$$

Preference values must be between 0 and 1. A value of 1 indicates maximum preference toward a product.

If the competitor preference  $H_2 = .69$  and  $H_1 = 1$  (max) then the overall  $\beta = .69/1 = .69$

# Consumer Utility and Preference

$$\beta = \frac{H_2}{H_1}$$

- Consumer Preference

$$H_i = \sum w_i y_i$$

$w_i$  = weight based on consumer preference characteristics, smaller than 1

$y_i$  = consumer utilities based on evaluation, can be changed to meet specific preference values. Range between 0 and 1. 1 is 100% satisfaction in the product

# Consumer Utility and Preference

## ■ Determining weights

1. Identify Important Characteristics for general oxygen supply for a hospital
2. Determine consumer importance placed on characteristics through surveys
3. Characteristic relation to product properties
4. Determine weights to each characteristic from importance surveys



# Consumer Utility and Preference

- Important consumer characteristics for hospital design and weights assigned to them.



Characteristics	Weights (wi)
Noise	0.175
Ease of Use	0.147
Appearance	0.112
Frequency of Maintenance	0.184
Reliability	0.205
Durability	0.177

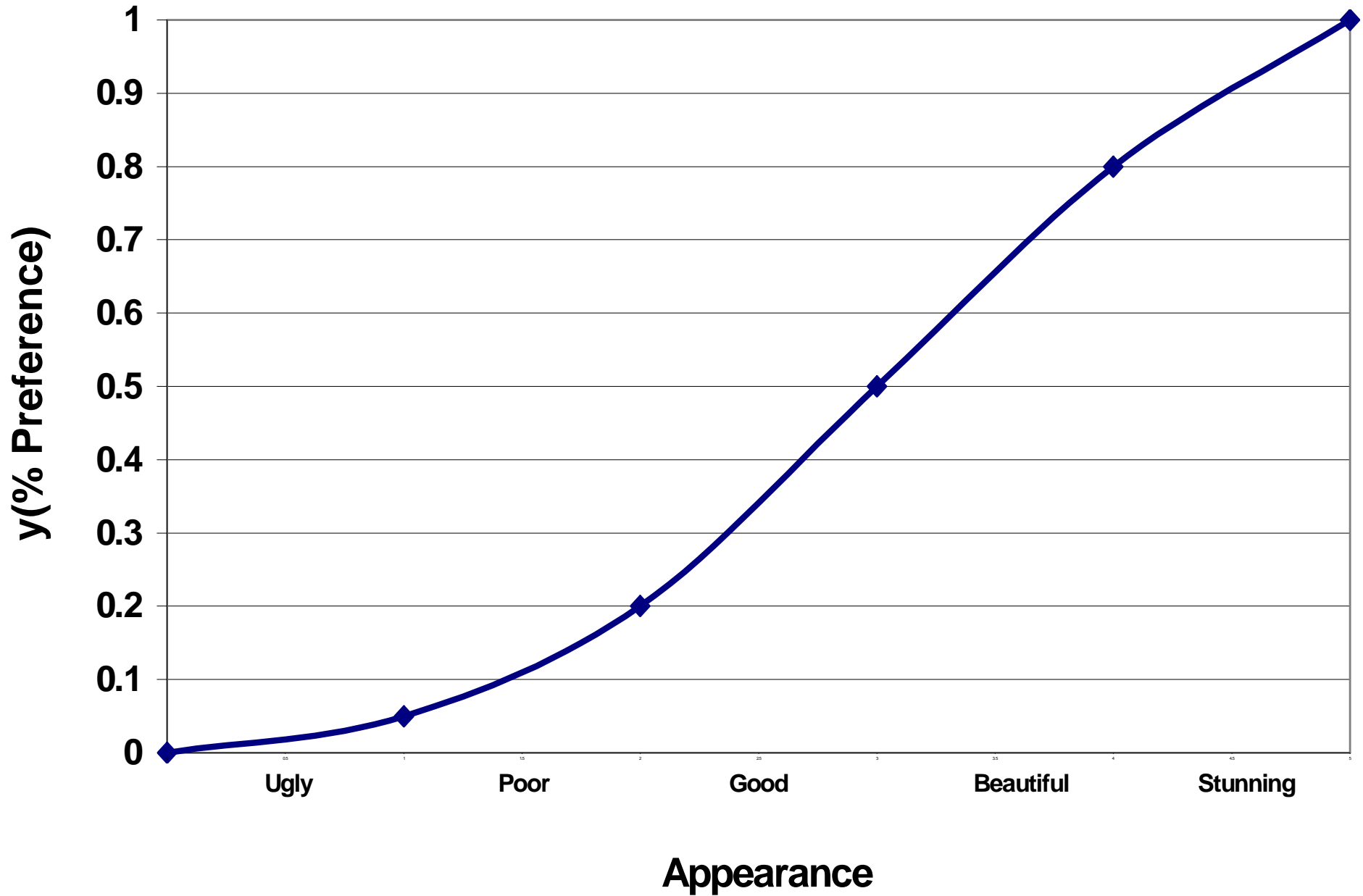
# Consumer Utility and Preference

Determining  $y_i$  (%preferences) of consumer values

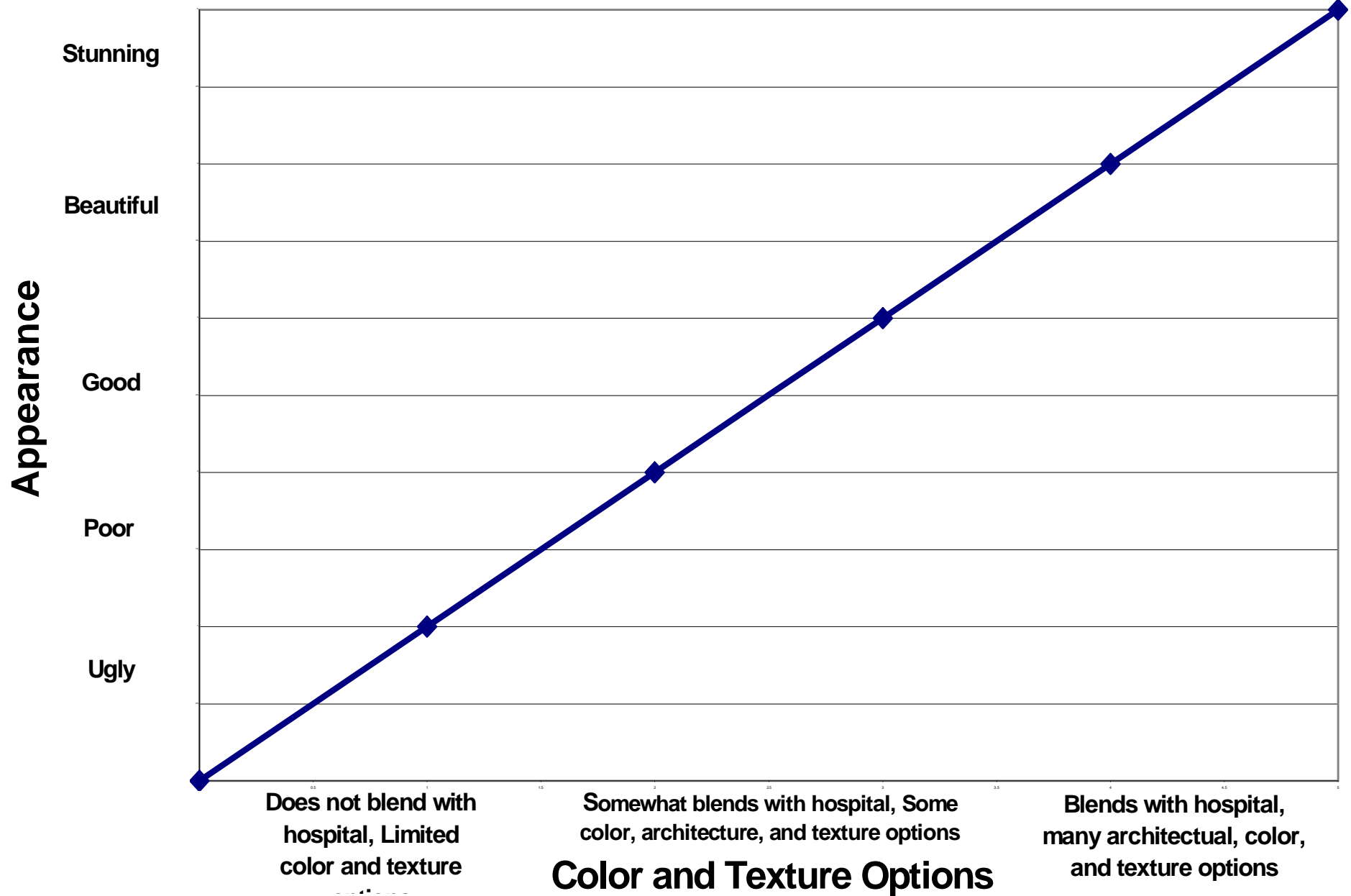
$$H_i = \sum w_i y_i$$

1. Develop expression between %preference and words used to describe each characteristic by consumer description.
2. Relates the characteristic descriptions to physical attributes.
3. Combine the first two expressions to yield a % preference of characteristic versus physical attributes.

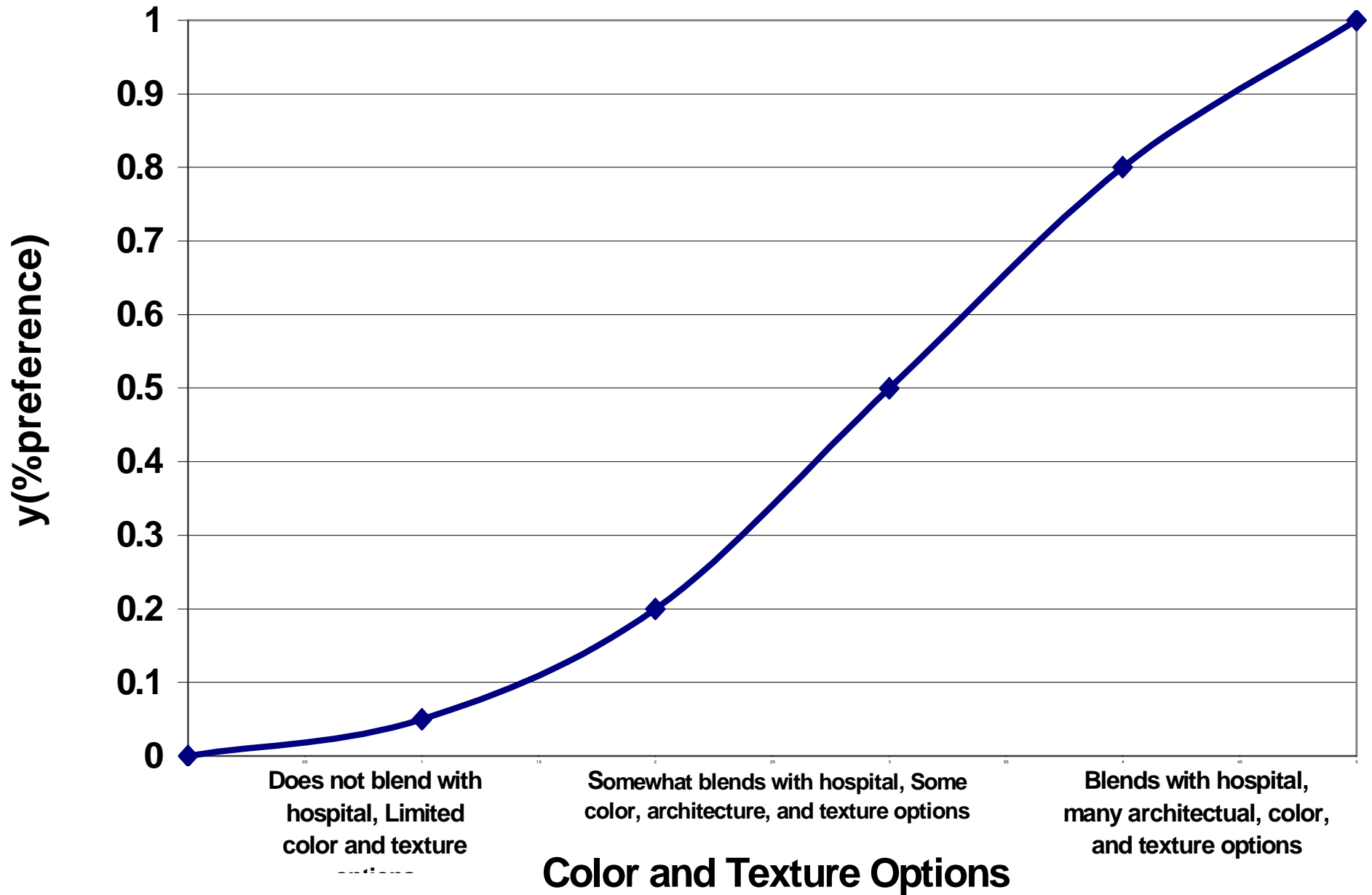
# % Preference for Appearance Characteristic



# Appearance Characteristic



# Appearance Characteristic



# Consumer Utility and Preference

## *Appearance*

- Utility function (yi) generated

$$Y(\% \text{preference}) = -0.0134x^3 + 0.1248x^2 - 0.0888x + 0.0063 \quad \text{where } x = \text{Color/Texture}$$

The appearance of the oxygen concentrator depends on the outer casing.

# Consumer Utility and Preference

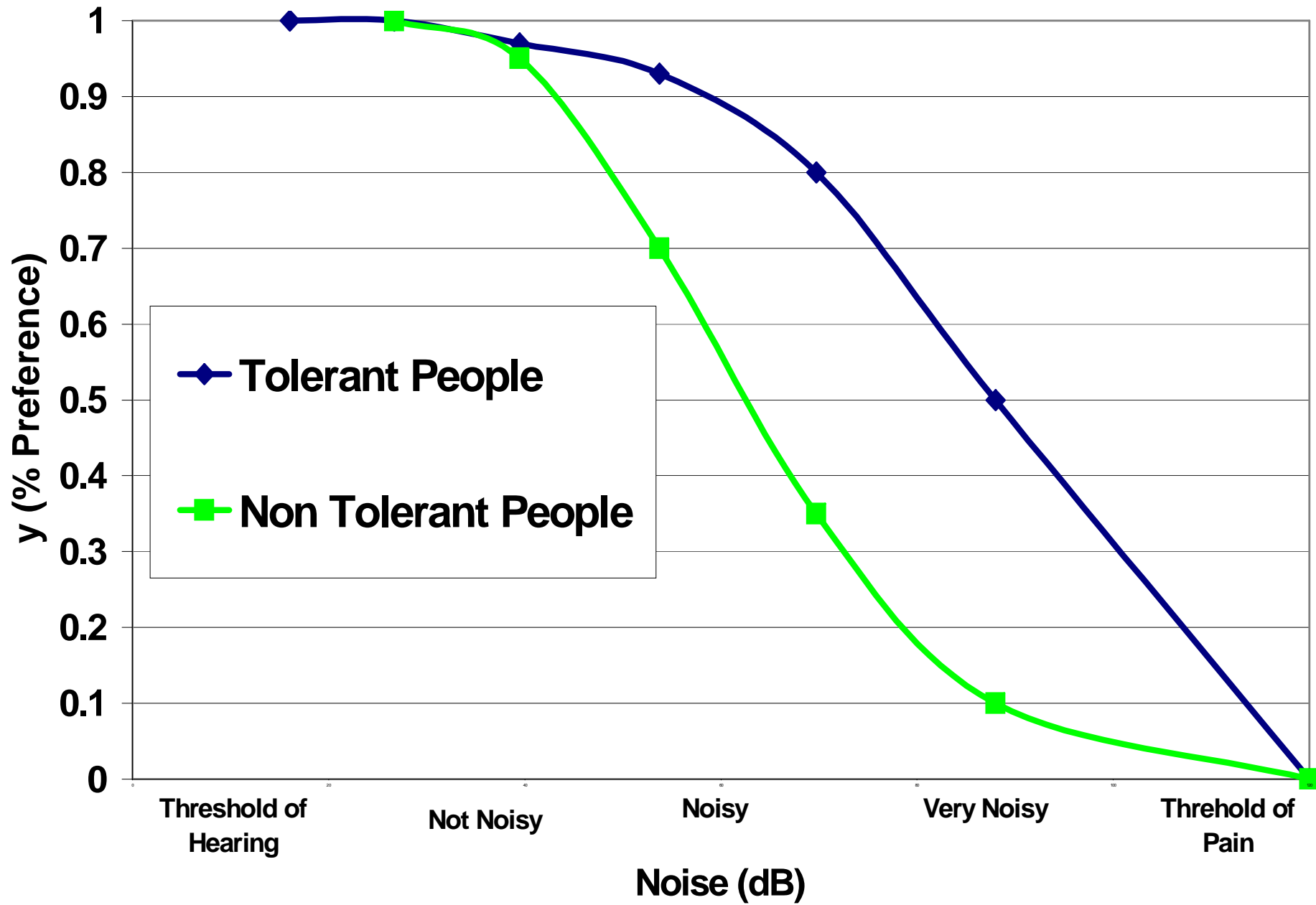
## *Appearance*

- To draw in the most consumers, 3 types of siding materials were looked at: Veneer, Aluminum, and Vinyl.



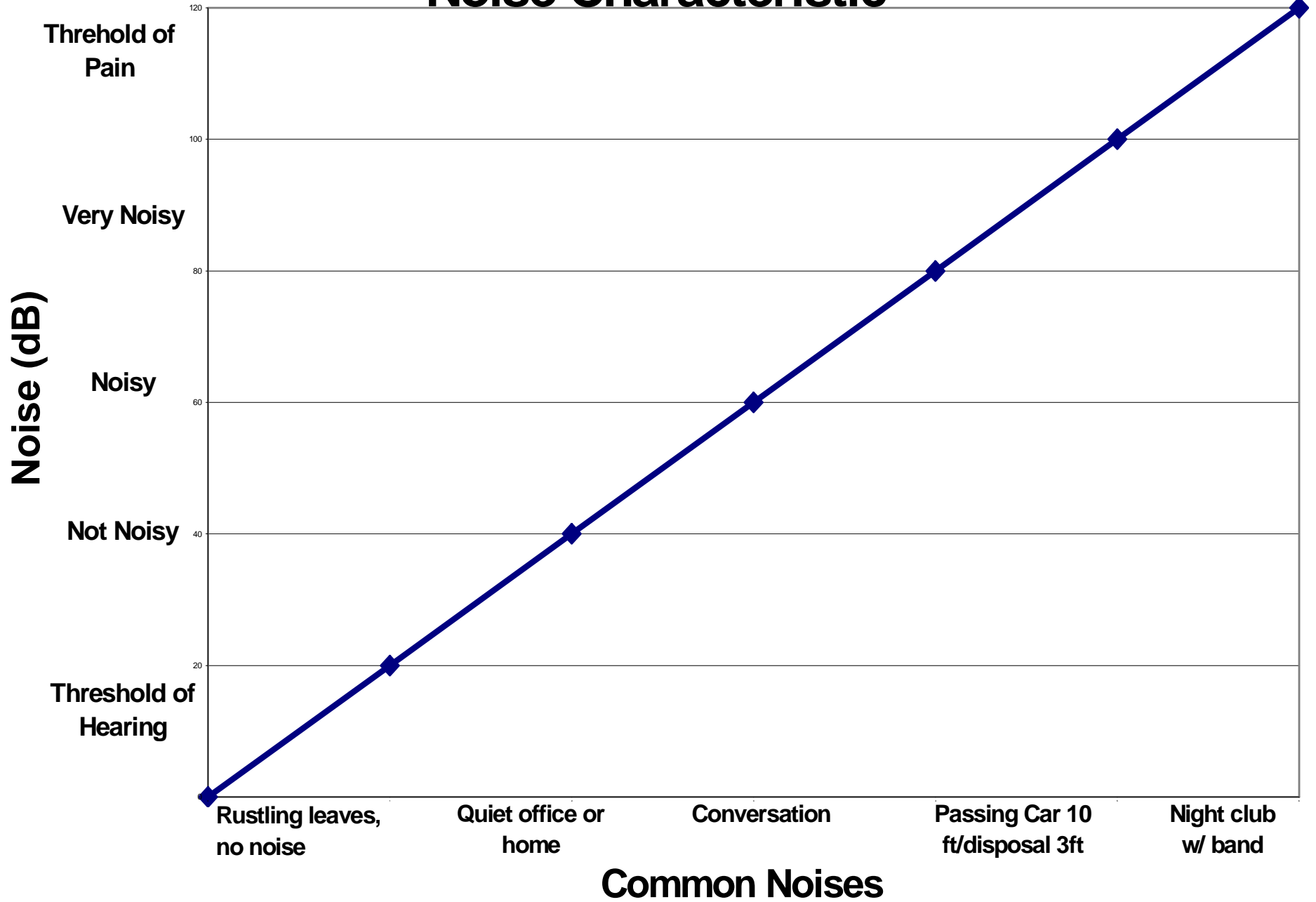
Material	Quoted Price	Total Cost
Vinyl Siding	\$1.6/ sq ft [30]	\$1,760
Aluminum Siding	\$1.7/ sq ft [30]	\$1,870
Veneer Stone Siding	\$3.5/ sq ft [31]	\$3,850

# % Preference for Noise Characteristic

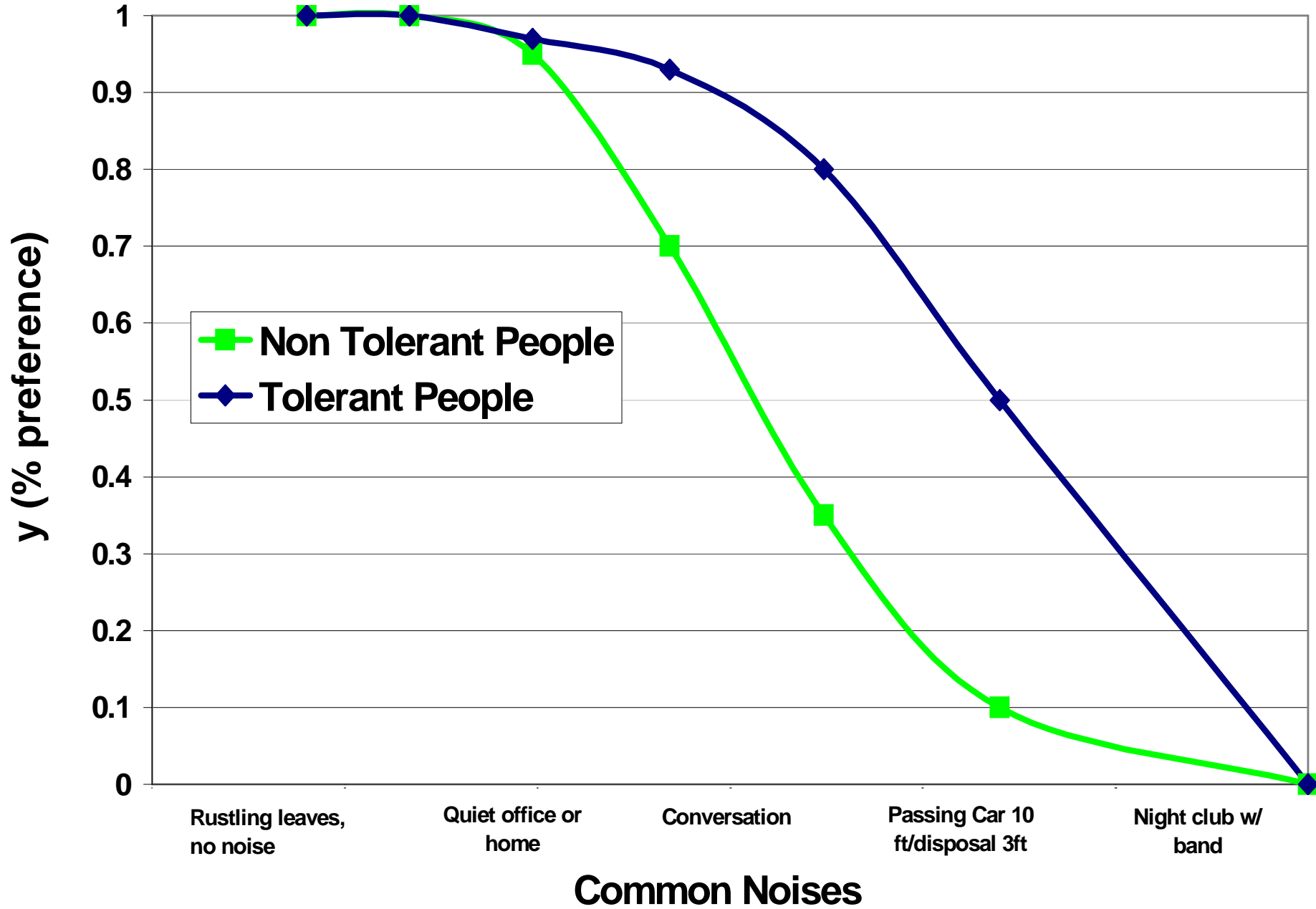




# Noise Characteristic



# Noise Characteristic



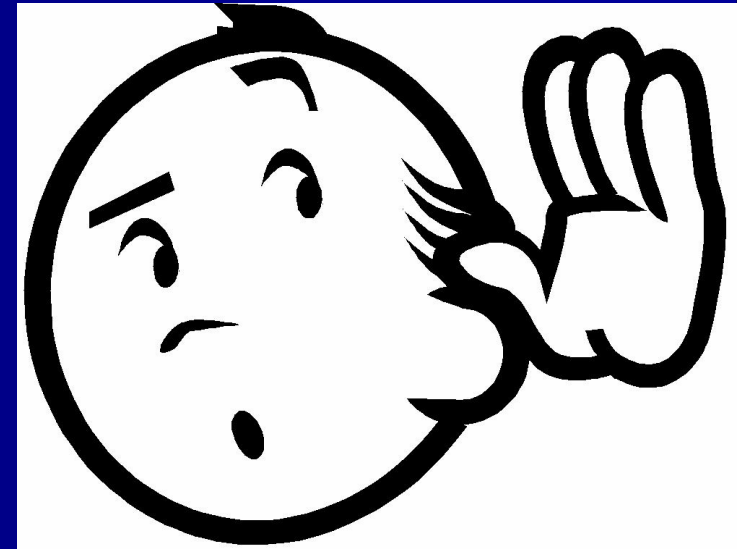
# Consumer Utility and Preference

## *Noise*

- Utility function (yi)  
generated

$$Y(\% \text{preference}) = -4E-06x^3 - 0.0007x^2 + 0.0278x + 0.724$$

where  $x$ (common noise)



# Consumer Utility and Preference

## *Noise*

- To draw in the most consumers, a layer of noise soundproofing foam will be added to the casing of the concentrator.



Material	Reduction %	Total Cost (\$)
Ultra Barrier	95	10141
Quiet Barrier	90	4412
Econo Barrier	80	2119
Sound Proof Foam	65	2406

# Consumer Utility and Preference

## *Ease of Use (amount of training)*

- Utility Function

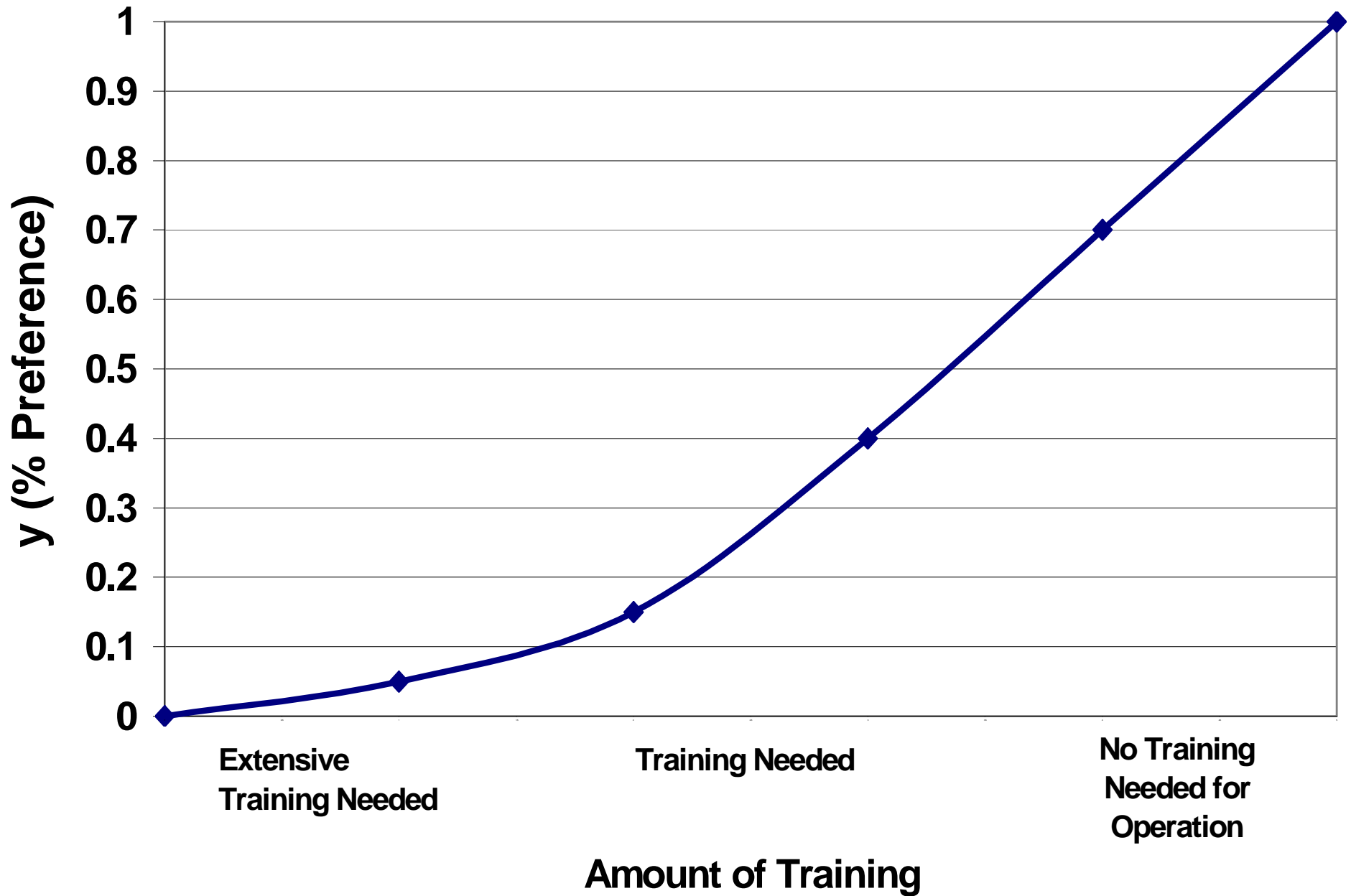
$$Y(\% \text{preference}) = 0.0366x^2 + 0.0227x - 0.0089$$

where  $x$  = (Training Needed)

If no training is needed  
than the hospital design  
is easy for anyone to  
use.



# % Preference for Ease of Use Characteristic



# Consumer Utility and Preference

## *Reliability (MTBF)*

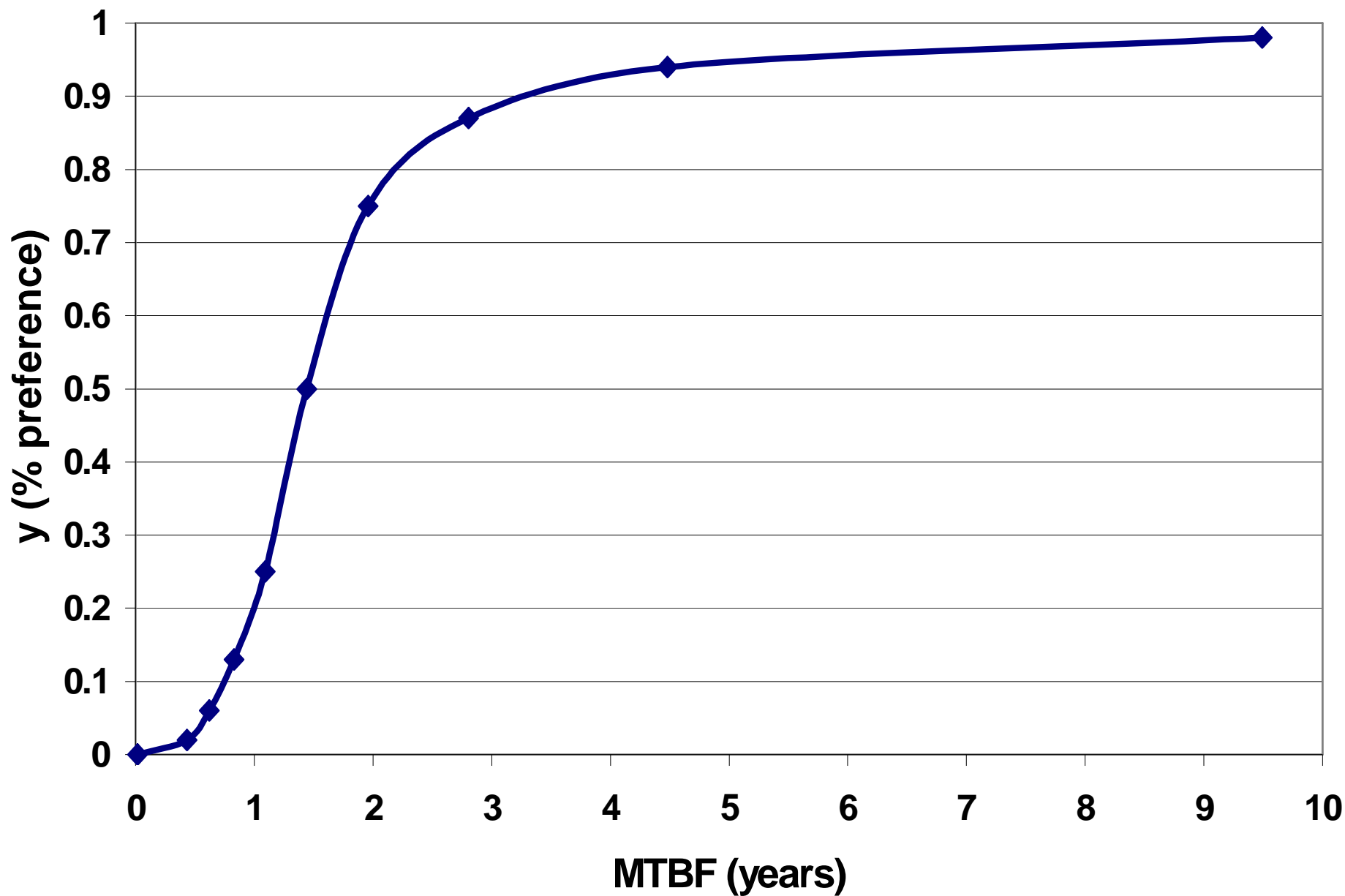
- Utility function (yi)  
generated

$$Y(\% \text{preference}) = 0.0037x^3 - 0.0796x^2 + 0.5394x - 0.159$$

where  $x(\text{MTBF})$



# % Preference for Reliability Characteristic





# Consumer Utility and Preference

## *Manipulation:*

Increase consumer preference by including parts with large MTBF values.

Adding a backup unit to the primary unit will increase reliability. If one unit breaks down, the other unit will turn on.



# Consumer Utility and Preference

## *Durability (time to revamp)*

- Utility function (yi) generated

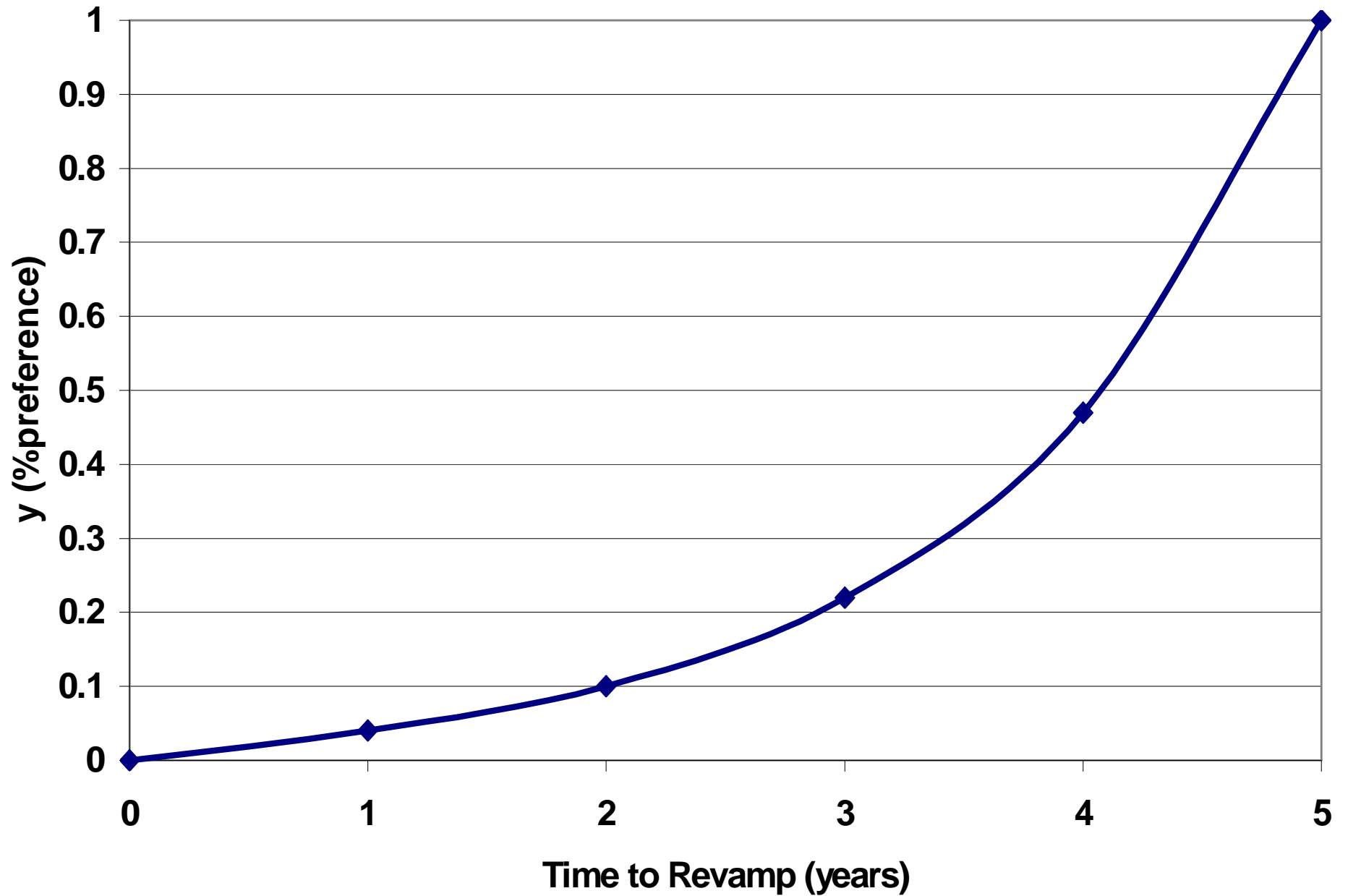
$$Y(\% \text{preference}) = 0.014x^3 - 0.0475x^2 + 0.0881x - 0.0037$$

where x(Time to Revamp)

- Manipulation: Increase consumer preference by including valves and compressors with long term resistance to wear.



## % Preference for the Durability Characteristic



# Consumer Utility and Preference

*Maintenance(visits per year)*  
Utility function (yi) generated

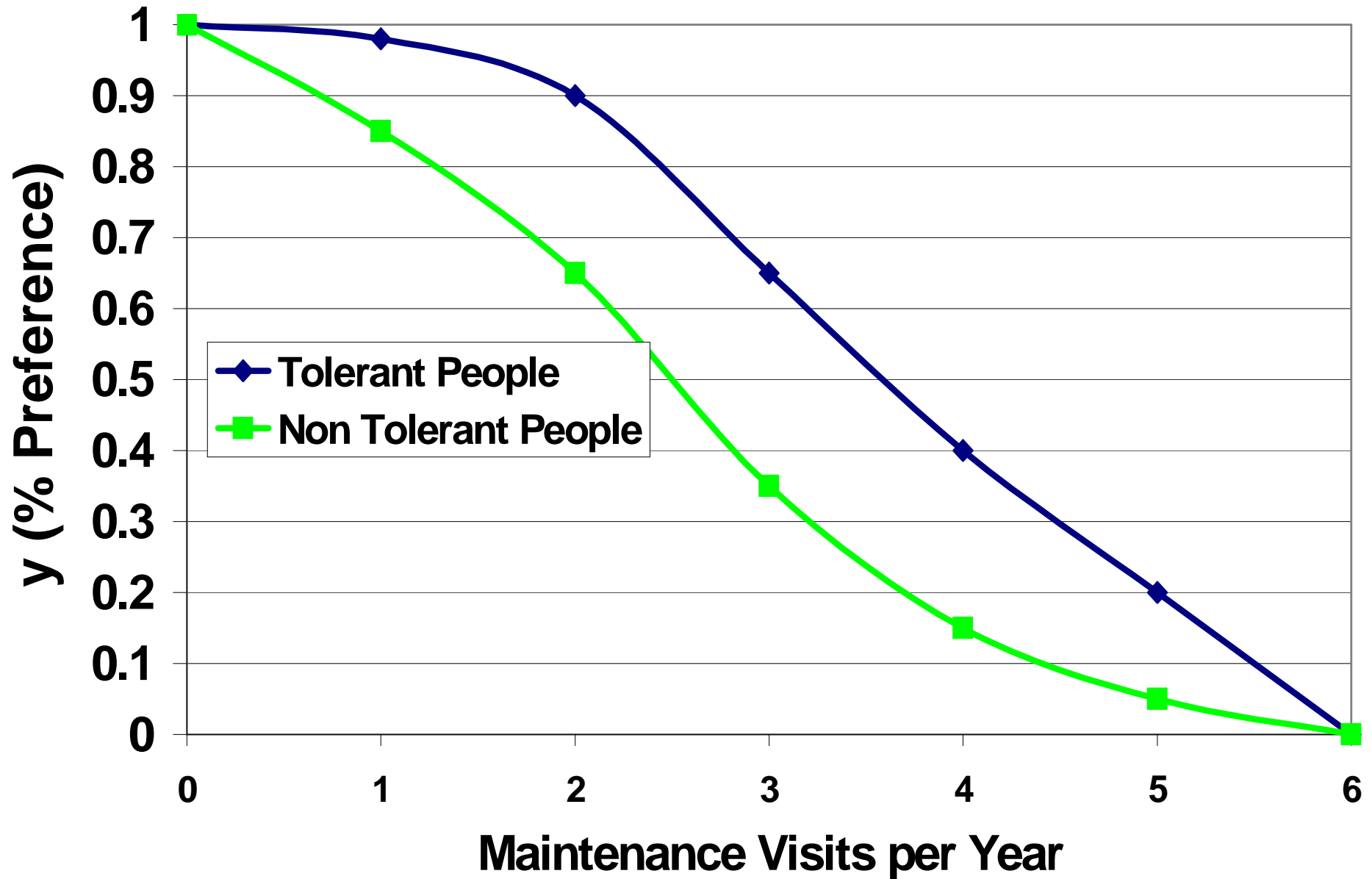
$$Y(\% \text{preference}) = -0.0083x^3 - 0.0607x^2 - 0.1012x + 1.0036$$

where  $x$ (Maintenance visits/year)

Manipulation: Greater MTBF leads to less maintenance.



# % Preference for Frequency of Maintenance Characteristic



# Consumer Utility and Preference

All utility functions are used to find % preference to be multiplied by characteristic weights to achieve the preference value.

$$Y(\text{Appearance}) = -0.0134x^3 + 0.1248x^2 - 0.0888x + 0.0063$$

$$Y(\text{Noise}) = -4E-06x^3 - 0.0007x^2 + 0.0278x + 0.724$$

$$Y(\text{Ease of Use}) = 0.0366x^2 + 0.0227x - 0.0089$$

$$Y(\text{Reliability}) = 0.0037x^3 - 0.0796x^2 + 0.5394x - 0.159$$

$$Y(\text{Durability}) = 0.014x^3 - 0.0475x^2 + 0.0881x - 0.0037$$

$$Y(\text{maintenance}) = -0.0083x^3 - 0.0607x^2 - 0.1012x + 1.0036$$

$$H_i = \sum w_i y_i$$

# Business Model

Competitor (liquid oxygen)	% Preference (yi)	Preference/Characteristic (Hi)
Noise	0.930	0.163
Ease of Use	0.950	0.140
Appearance	0.580	0.065
Frequency of Maintenance	0.360	0.066
Reliability	0.900	0.185
Durability	0.760	0.135
		<b>0.753</b>

Now found competitor H2 value can vary oxygen product to produce several new preference values H1 for different  $\beta$  values.

$$\phi(d_1) = p_1 d_1 - \left(\frac{\alpha}{\beta}\right)^\rho p_2 \left[\frac{Y - p_1 d_1}{p_2}\right]^{1-\rho} d_1^\rho = 0$$

Example Designs	
	Beta Values
Design1	0.85
Design2	0.92
Design3	0.95
Design4	0.97
Design5	1.05
Design6	1.12

# Business Model for Hospital Design





# Business Model

## Goals

- Determine  $\beta$  value that will maximize NPV at the best price for design.
- Determine the effect of varying  $\alpha$ (knowledge) with time with a set  $\beta$  value.

# Business Model

**Determining P1 and D1:** Example of prices and demands from consumer utility maximization with Beta=.85

$$p_1 d_1 - \left( \frac{\alpha}{\beta} \right)^\rho p_2 \left[ \frac{Y - p_1 d_1}{p_2} \right]^{1-\rho} d_1^\rho = 0$$

Price	Demand
150000	291
175000	202
200000	140
225000	98
250000	69
275000	50
300000	36
325000	27
350000	20

# Business Model

Items now needed to find NPV

- Total Product Costs
  - Raw Materials
  - Variable Production Costs
  - Administrative Costs
  - Advertising Costs
  - Distribution Costs
  - Fixed Charges
- TCI
- Total Equipment Costs



# Business Model

**Total Product Costs per year**  
Raw materials (depend on demand)

## Raw Materials Cost

	Basis for Estimate	Rate or Quantity	\$
Silica Gel	\$.22/100g quote 20 units sold in first year	920 g	\$20
LiAgX Zeolite	\$.4/100g quote 20 units sold in first year	4130 kg	\$165,200
Silver Zeolite A	\$.4/100g quote 20 units sold in first year	1230 kg	\$49,200
Quiet Barrier Noise Proof Foam	Quote: \$361/sheet	16 sheets to cover casing of unit	\$115,520
Vinyl Siding	Quote: \$1.6/sq ft	1400 sq ft to cover	\$44,800
		<b>Total Raw Materials Cost</b>	<b>\$214,420</b>

# Business Model

## Total Product Costs

- Variable Production Costs (utilities, supplies, maintenance)

### Variable Production Costs

Utilities	Basis for Estimate	Rate or Quantity	
<b>Electricity</b>	150 bulbs, 23W, full year operation	\$.13/kWh	\$3,884
	Office heating/cooling/electronics 900W/hr		\$1,157
<b>Water</b>	Assume 100 gal/day	\$1.98/1000 gal (Georgia cost)	\$723
<b>Operating Supplies (variable costs)</b>			
Pencils	12 BIC Mechanical Pencils \$5.50	Use 288 per year	\$132
Staples	Swingline \$1.50 per box	Use 3 boxes per year	\$5
Ink for Printer	\$60 per black/color ink combo package	Use 6 per year	\$360
Pens	12 Bic Pens \$5.50	Use 96 per year	\$44
Paper	\$33 per case of multipurpose paper	Use 2 per year	\$66
<b>Maintenance and repairs on building</b>		Estimate of .05 of FCI	\$1,150
<b>Total variable production costs</b>			<b>\$7,520</b>

# Business Model

## Total Product Costs

- Administrative Costs

<b>Administrative Costs</b>			
<b>Employees</b>	<b># employees</b>		
Engineers	1	Assume \$60,000 salary/year	\$60,000
Accountant	1	Assume \$30000 salary/year	\$30,000
Skilled Labor	2	Assume \$30000 salary/year	\$60,000
Traveling Salesman	1	Assume \$35000 salary/year	\$35,000
Secretary	1	Assume \$25000 salary/year	\$25,000
Traveling Maintenance	1	Assume \$35000 salary/year	\$35,000
		<b>Total Administrative Costs</b>	<b>\$245,000</b>

# Business Model

## Distribution and marketing expenses

Distribution and marketing expenses			
	Basis for Estimate	Rate or Quantity	
<b>Sales personnel expenses</b>	Assume visits 70% large hospitals = 175, only 3 day/ trip estimate, 35 trips/year		
	Airfare	\$400/trip	\$14,000
	Hotel	\$100/trip per day	\$10,500
	Food	\$50/trip per day	\$5,250
	Rental Car / Gas	\$80 per day for rent and gas	\$8,400
	<b>Total Sales Expenses per Year</b>		<b>\$38,150</b>
<b>Advertising</b>	Assume high advertising from calculations		Estimated \$100,000
	Brochures	\$1/brochure, send 50 to each hospital/year	\$12,500
	DVD	\$8/DVD, send 10 to each hospital/year	\$20,000
	Mailing expenses	Assume 10lb per box at \$20/box	\$10,000
	<b>Total Adversing Expenses (high advertisement rate)</b>		<b>\$42,500</b>
<b>Shipping</b>	20 units shipped in first year from demand es	\$.3/kg, unit weight ~ 16000kg	\$192,000
<b>Total Distribution and marketing expenses</b>			<b>\$272,650</b>

**Total Product Cost for First-Year  
Product: Pressure Swing Adsorption for Large Hospitals**

Operating time day/year	250		
Estimated units fabricated/year	20		
	<b>Basis for Estimate</b>	<b>Rate or Quantity</b>	<b>\$</b>
Silica Gel	\$ .22/100g quote 20 units sold in first year	1840 g	\$81
LiAgX Zeolite	\$.4/100g quote 20 units sold in first year	8260 kg	\$660,800
Silver Zeolite A	\$.4/100g quote 20 units sold in first year	2460 kg	\$196,800
Quiet Barrier Noise Proof Foam	Quote: \$361/sheet	16 sheets to cover casing of unit	\$115,520
Vinyl Siding	Quote: \$1.6/sq ft	1400 sq ft to cover	\$44,800
		<b>Total Raw Materials Cost</b>	<b>\$1,018,001</b>
<b>Variable Production Costs</b>			
<b>Utilities</b>			
<b>Electricity</b>	150 bulbs, 23W, full year operation	\$.13/kWh	\$3,884
	Office heating/cooling/electronics 900W/hr		\$1,157
<b>Water</b>	Assume 100 gal/day	\$1.98/1000 gal (Georgia cost)	\$723
<b>Operating Supplies (variable costs)</b>			
Pencils	12 BIC Mechanical Pencils \$5.50	Use 288 per year	\$132
Staples	Swingline \$1.50 per box	Use 3 boxes per year	\$5
Ink for Printer	\$60 per black/color ink combo package	Use 6 per year	\$360
Pens	12 Bic Pens \$5.50	Use 96 per year	\$44
Paper	\$33 per case of multipurpose paper	Use 2 per year	\$66
<b>Maintenance</b>	\$5000 per maintenance visit	Estimate 1/10 break down in year 1	\$10,000
		<b>Total variable production costs</b>	<b>\$10,607</b>
<b>Fixed Charges</b>			
<b>Warehouse</b>	<b>\$6.9/sq ft/year quote</b>	<b>3200 sq ft, Atlanta, Georgia (20% office)</b>	<b>\$22,080</b>
		<b>Total Fixed Charges</b>	<b>\$22,080</b>
<b>Administrative Costs</b>			
<b>Employees</b>	<b># employees</b>		
<b>Engineers</b>	1	Assume \$60,000 salary/year	\$60,000
<b>Accountant</b>	1	Assume \$30000 salary/year	\$30,000
<b>Skilled Labor</b>	2	Assume \$30000 salary/year	\$60,000
<b>Traveling Salesman</b>	1	Assume \$35000 salary/year	\$35,000
<b>Secretary</b>	1	Assume \$25000 salary/year	\$25,000
<b>Traveling Maintenance</b>	1	Assume \$35000 salary/year	\$35,000
		<b>Total Administrative Costs</b>	<b>\$245,000</b>
<b>Distribution and marketing expenses</b>			
<b>Sales personnel expenses</b>	Assume visits 70% large hospitals = 175, only 3 day/ trip estimate, 35 trips/year		
	Airfare	\$400/trip	\$14,000
	Hotel	\$100/trip per day	\$10,500
	Food	\$50/trip per day	\$5,250
	Rental Car / Gas	\$80 per day for rent and gas	\$8,400
		<b>Total Sales Expenses per Year</b>	<b>\$38,150</b>
<b>Advertising</b>	Assume high advertising from calculations	Estimated \$100,000	
	Brochures	\$1/brochure, send 50 to each hospital/year	\$12,500
	DVD	\$8/DVD, send 10 to each hospital/year	\$20,000
	Mailing expenses	Assume 10lb per box at \$20/box	\$10,000
		<b>Total Advertising Expenses (high advertisement rate)</b>	<b>\$42,500</b>
<b>Shipping</b>	20 units shipped in first year from demand es	\$.3/kg, unit weight ~ 16000kg	\$192,000
		<b>Total Distribution and marketing expenses</b>	<b>\$272,650</b>
		<b>Total Product Cost</b>	<b>\$1,568,337</b>



# Business Model

- Now find TCI

## Capital Investment for Hospital Design

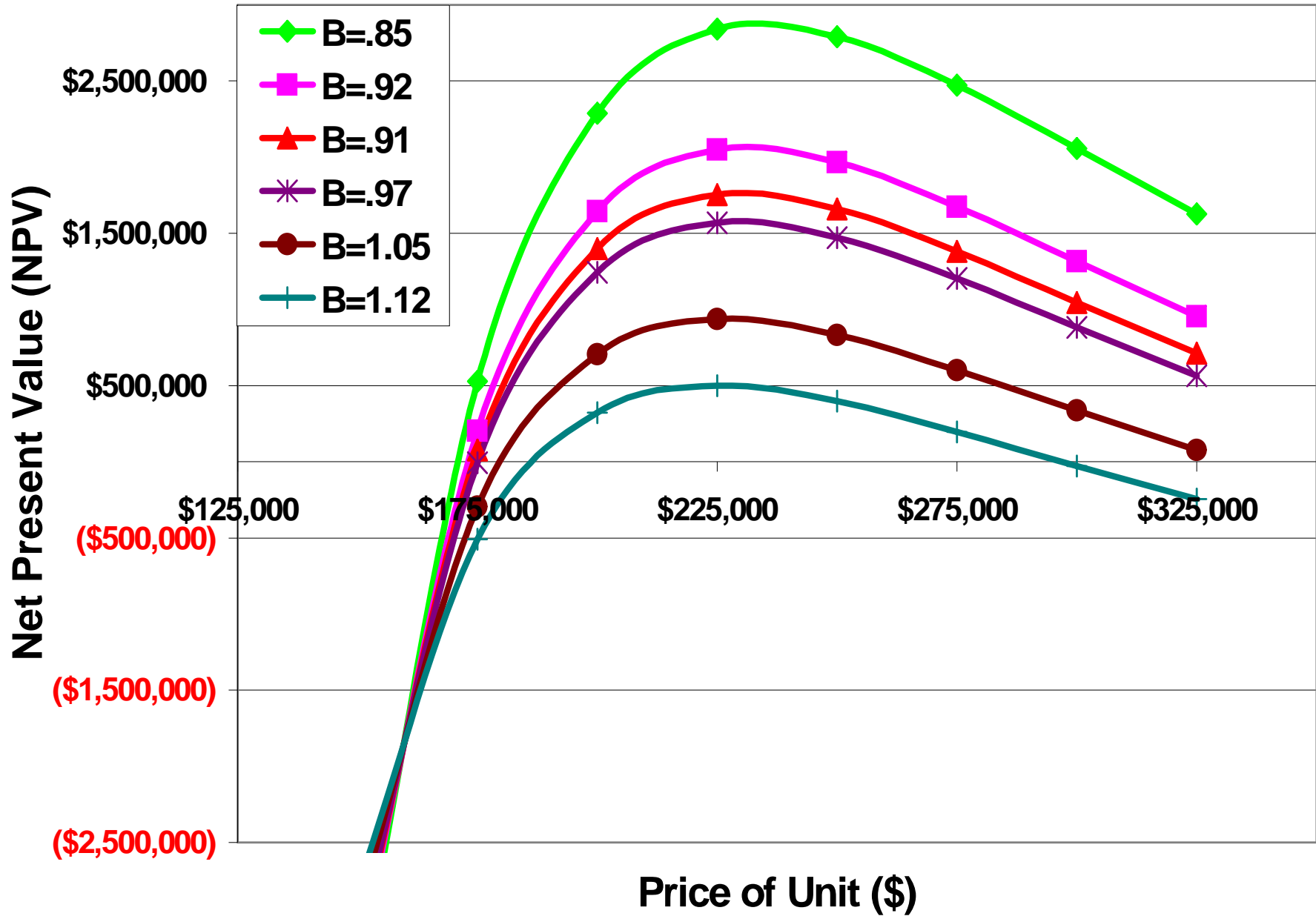
		Assumptions	Costs
<b>Office Furniture and Related Equipment</b>		<b>Quantity</b>	
Desks	\$250/desk (office depot)	4	\$1,000
Chairs	\$115/chair (office depot)	6	\$2,760
Phones	\$60/phone (multi line) (office depot)	6	\$360
Computers	\$800/computer (Dell Precision)	4	\$3,200
Office Supplies (stapler, rulers, paper)	\$300 for all supplies	N/A	\$150
Printer/Copier/Fax Machine	\$300 (Intellifax-400e) (office depot)	1	\$300
House keeping supplies (Vaccum, Mop)	\$200 (Dirt Devil - Bagless Upright)	1	\$300
Tools including nuts and bolts	\$3000/tool set (home depot)	3	\$9,000
Bobcat Forklift	\$3000 used price	1	\$3,000
<b>Total estimated fixed capital investment</b>			<b>\$20,070</b>
<b>Working Capital</b>		15% of TCI	<b>\$3,542</b>
<b>Total Capital Investment</b>			<b>\$23,612</b>

# Business Model

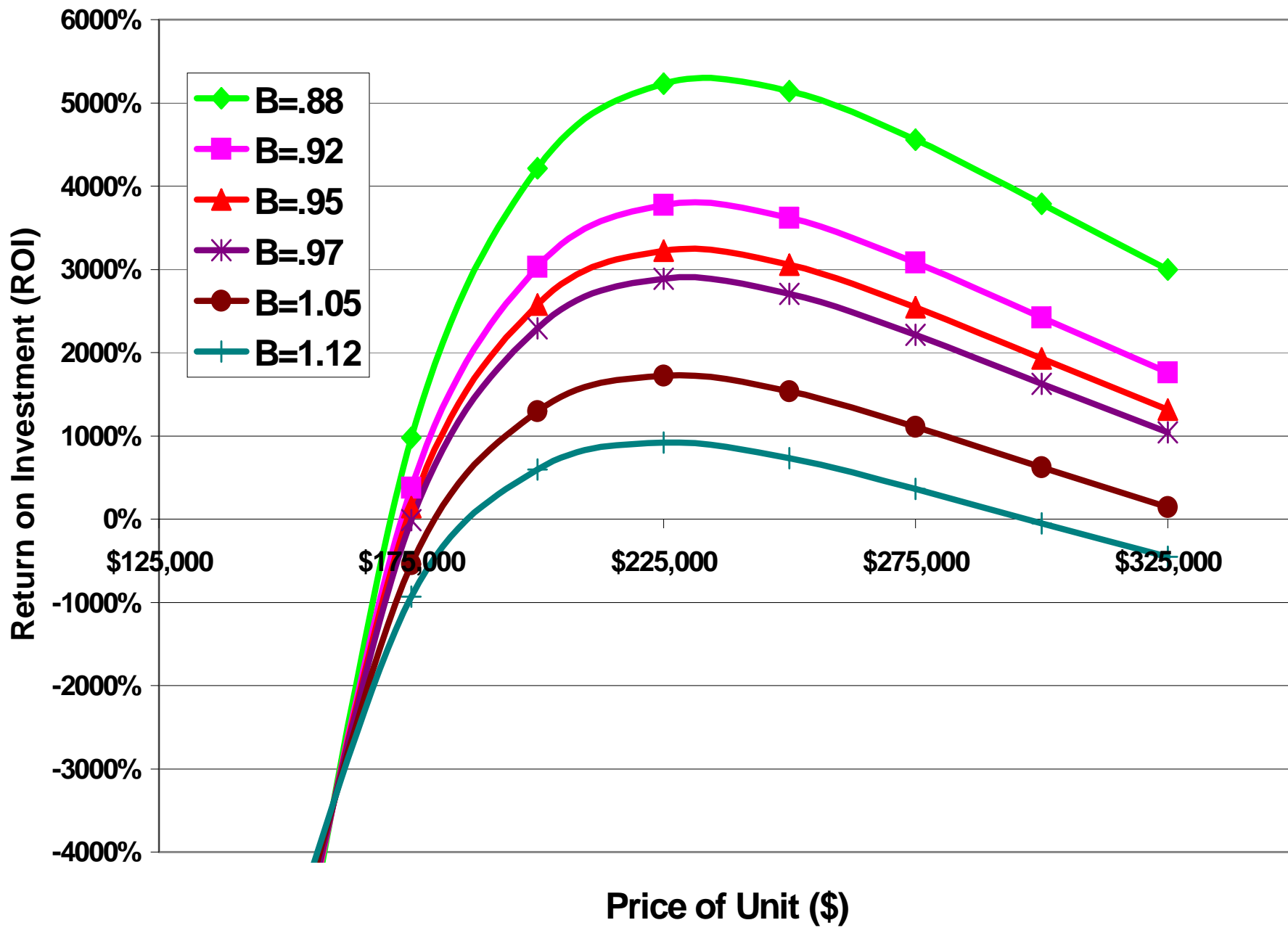
## ■ Lastly, Equipment Costs

<b>Estimation of Equipment Cost of 1 Unit</b>			
	<b>Basis for Estimate</b>	<b>Quantity</b>	<b>Equipment Costs</b>
<b>Nitrogen Removal Column</b>	Quote	4	\$32,000
<b>Drying Column</b>	Quote	1	\$200
<b>Palatek Compressor 200UD</b>	Quote: \$9800	2	\$19,600
<b>Palatek Compressor H30D7</b>	Quote: \$5000/unit	2	\$10,000
<b>High Pressure Storage Tank</b>	Fig.12.53 in P&T	1	\$12,000
<b>3 Way Control Valve</b>	Quote: \$700/unit	8	\$5,600
<b>Control Computer</b>	Quote	1	\$600
<b>Total Equipment Costs</b>			<b>\$80,000</b>

# NPV v Price



# ROI v Price



# Business Model

## Results:

- NPV over 5 year span = \$2,800,000
- Optimal  $\beta = .85$
- Price of unit \$250,000
- ROI for 1<sup>st</sup> year = 5200%

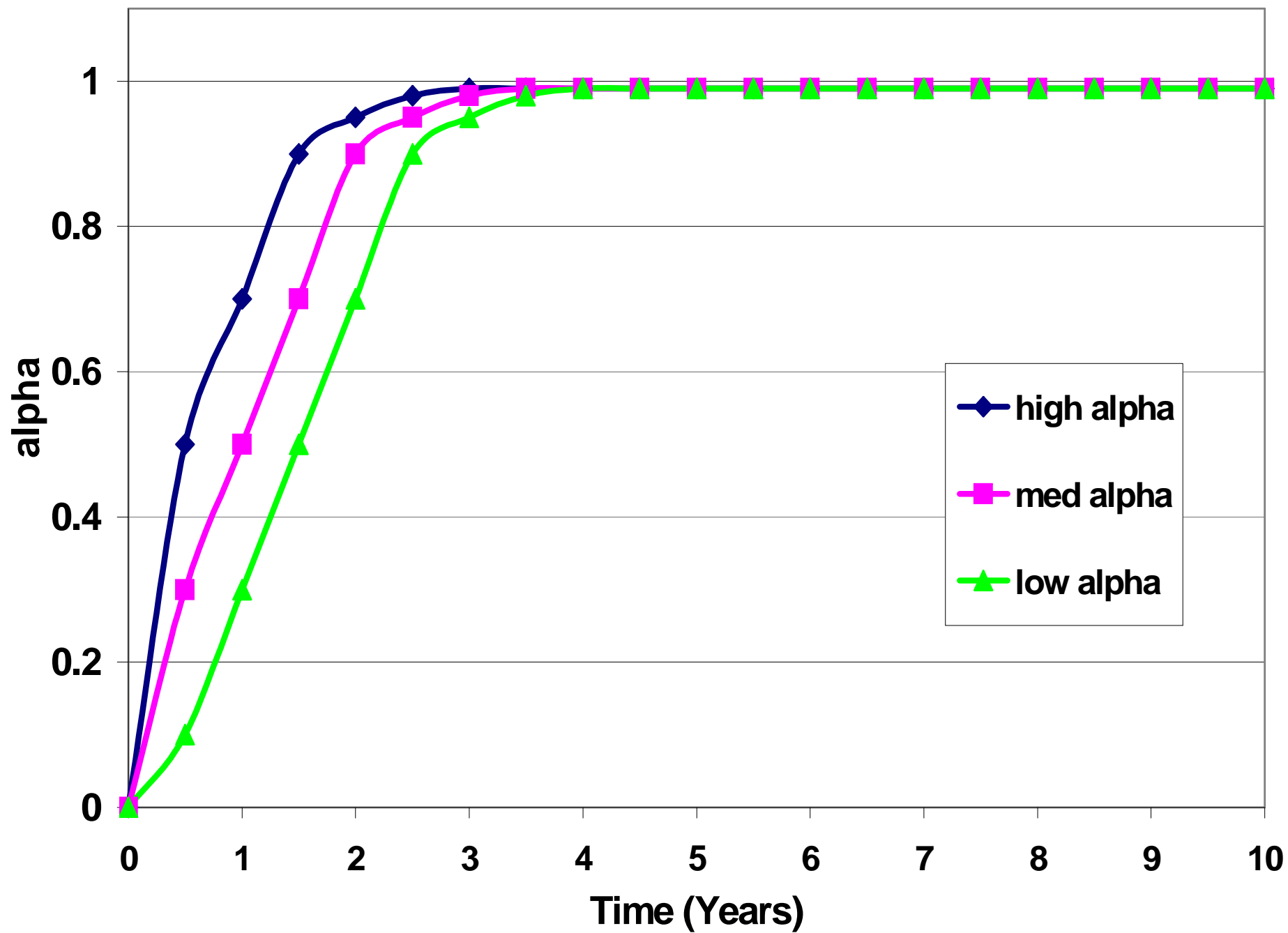
# Business Model

*Varying  $a$  (consumer knowledge) with Time*

# Business Model

## Goals

- Now find knowledge/advertising as a function of time
- Assume full consumer knowledge within 2 years of high advertising.





# Business Model

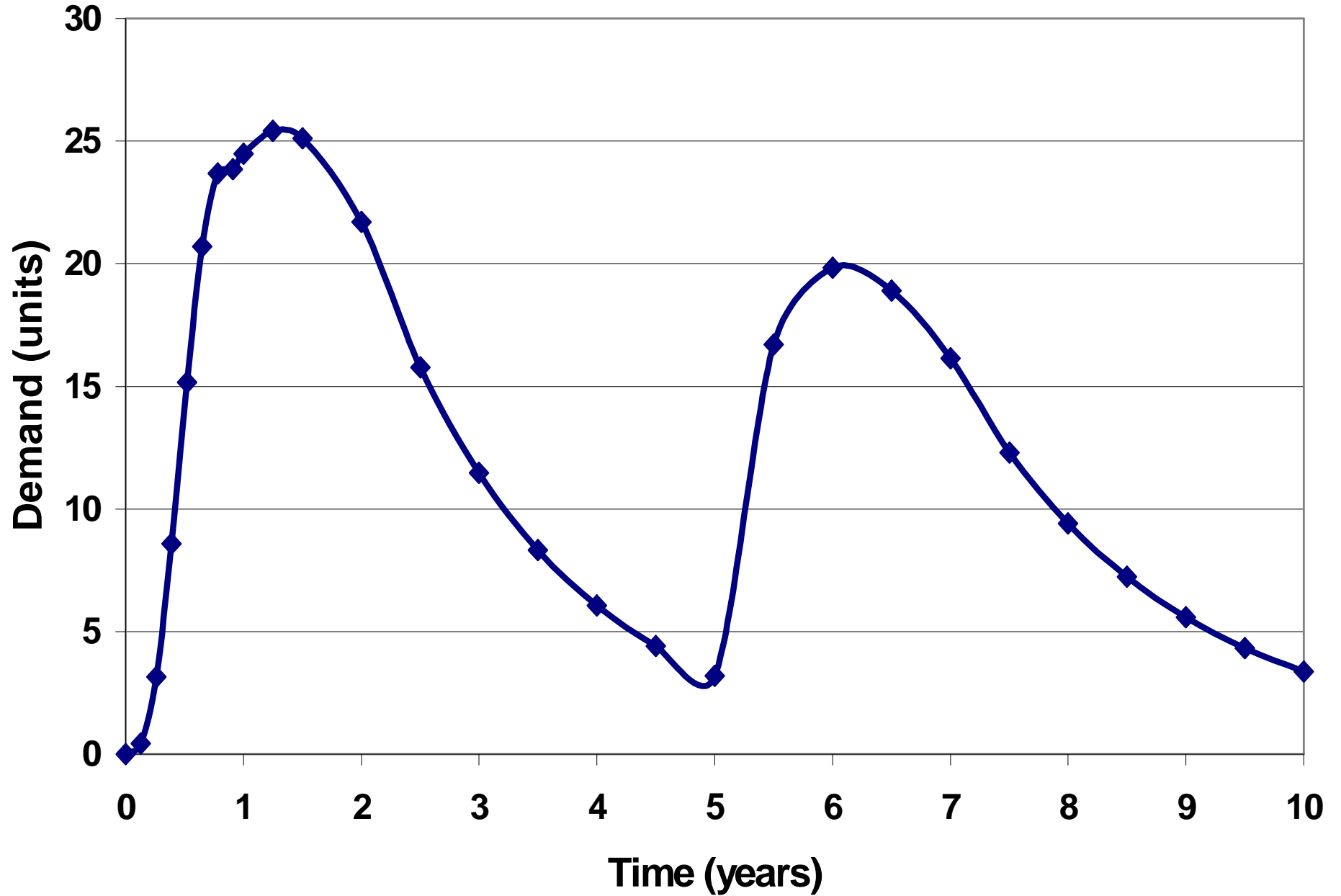
## Work Completed:

- Vary alpha with time with optimal beta and price.

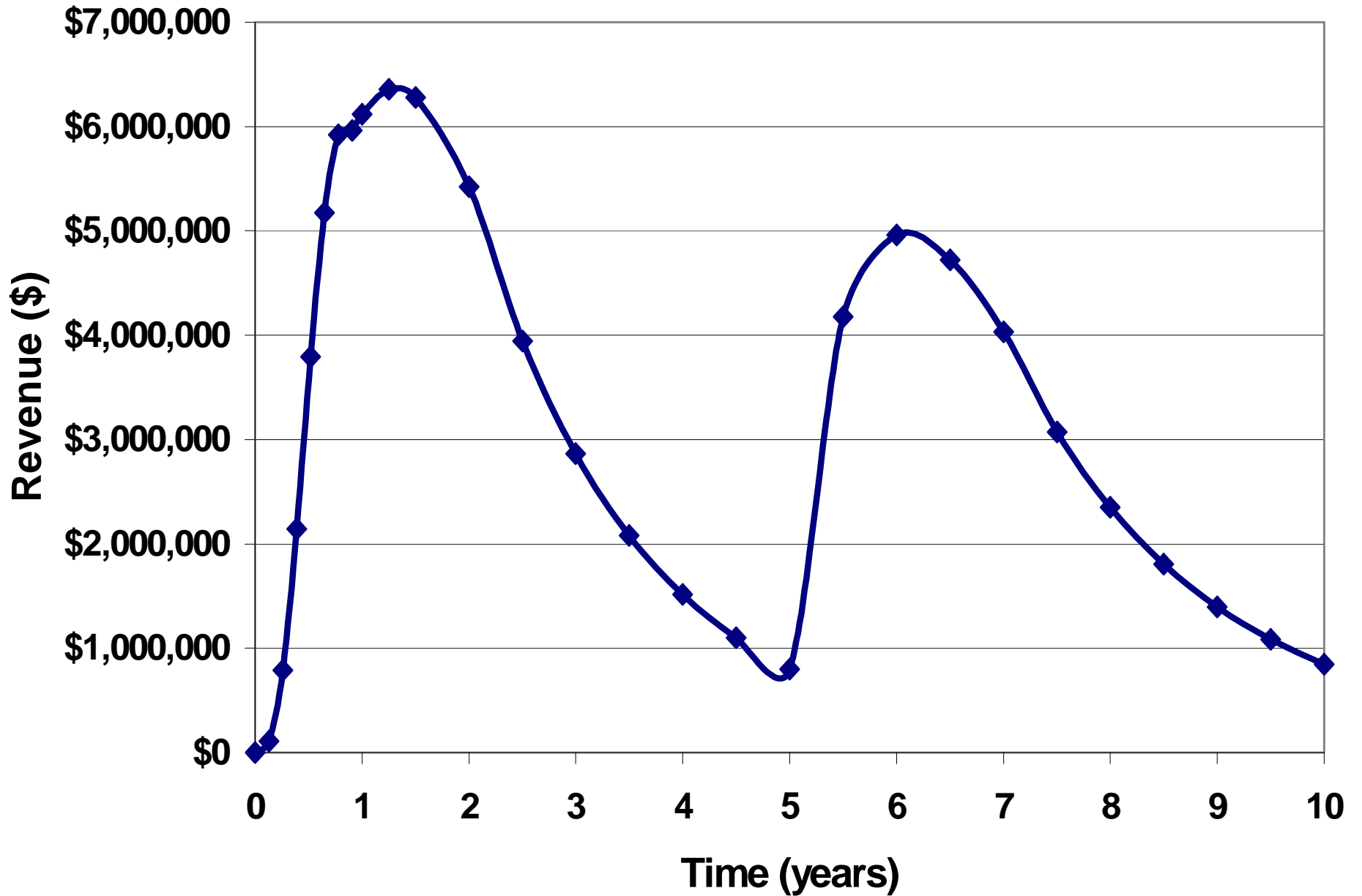
## ■ Graphs to Plotted:

- Revenue versus Time
- Demand versus Time
- NPV versus Time
- ROI versus Time

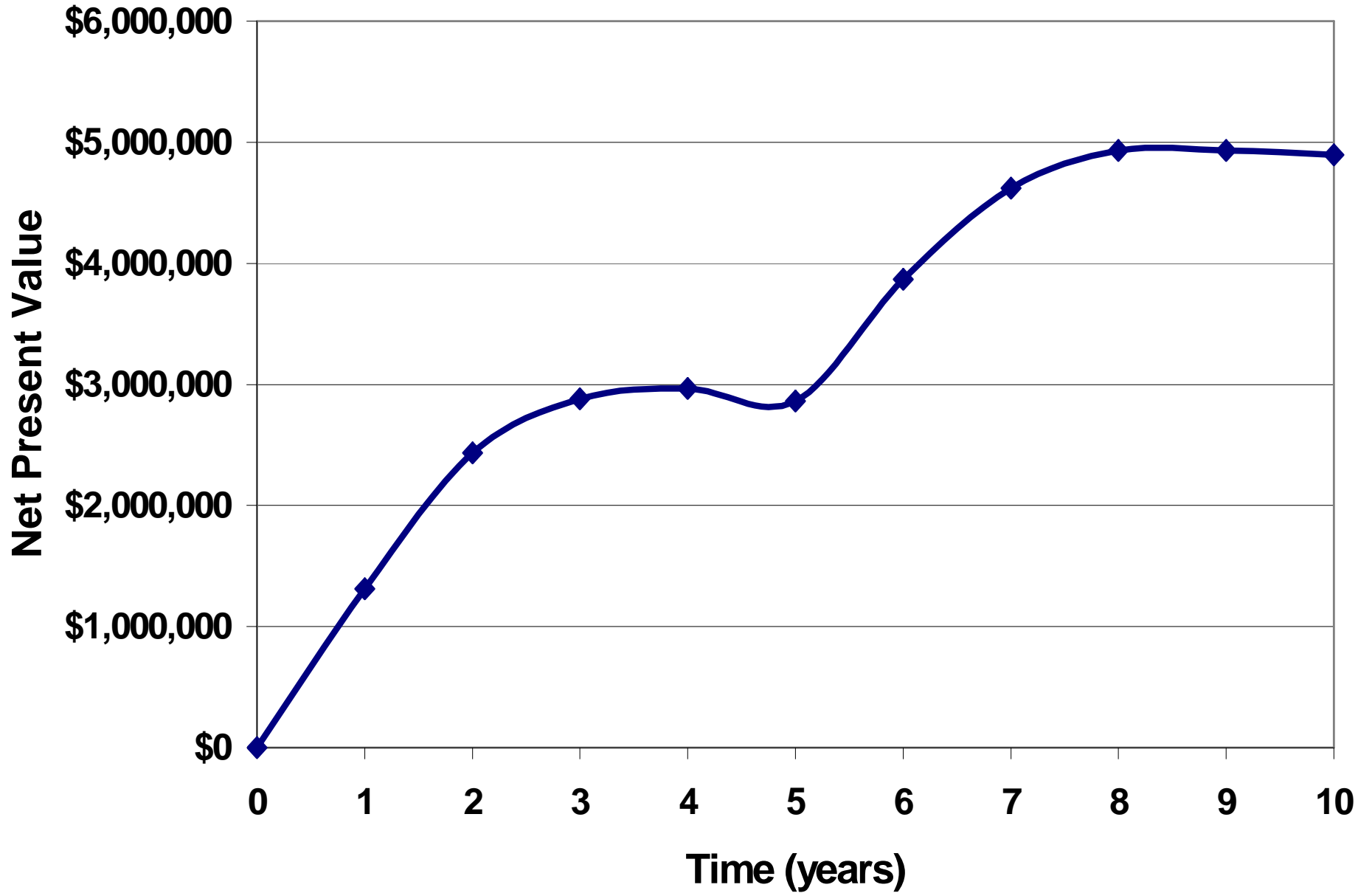
### Demand v Time (varying alpha)



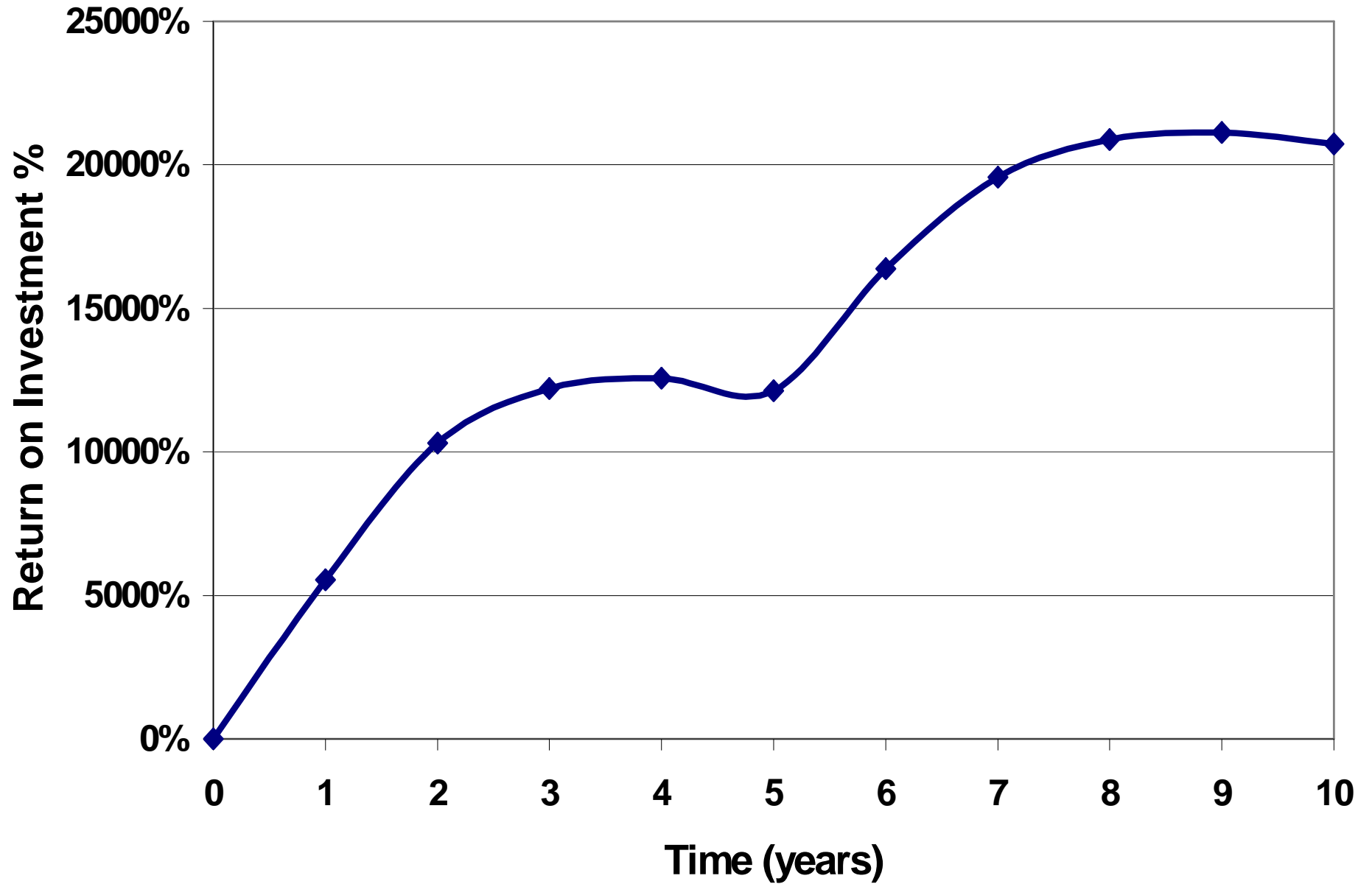
# Revenue v Time (Varying alpha)



# NPV v Time (varying alpha)



# ROI v Time (Varying Alpha)

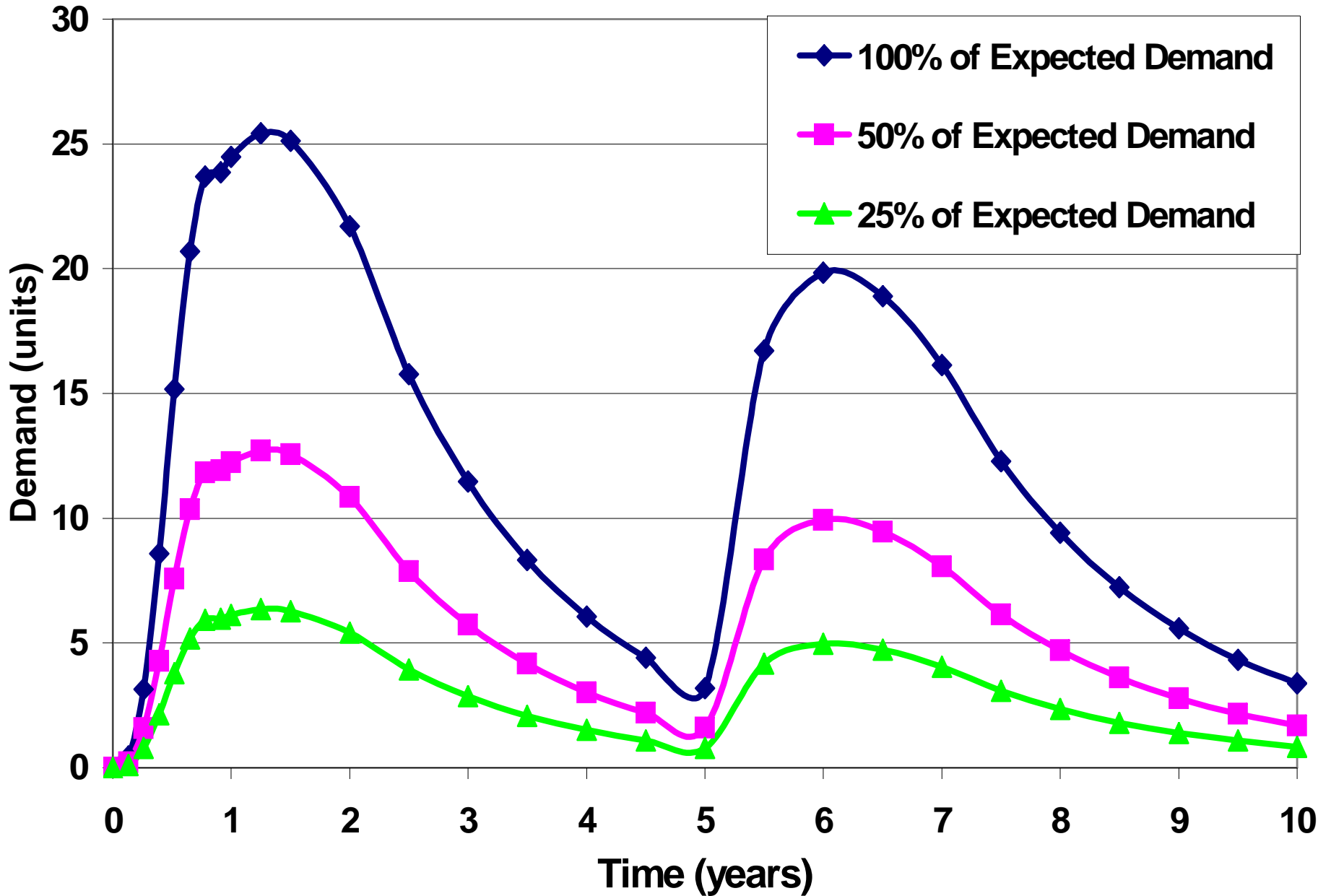


# **Preliminary Risk Estimates of Oxygen Concentrator**

# Risk

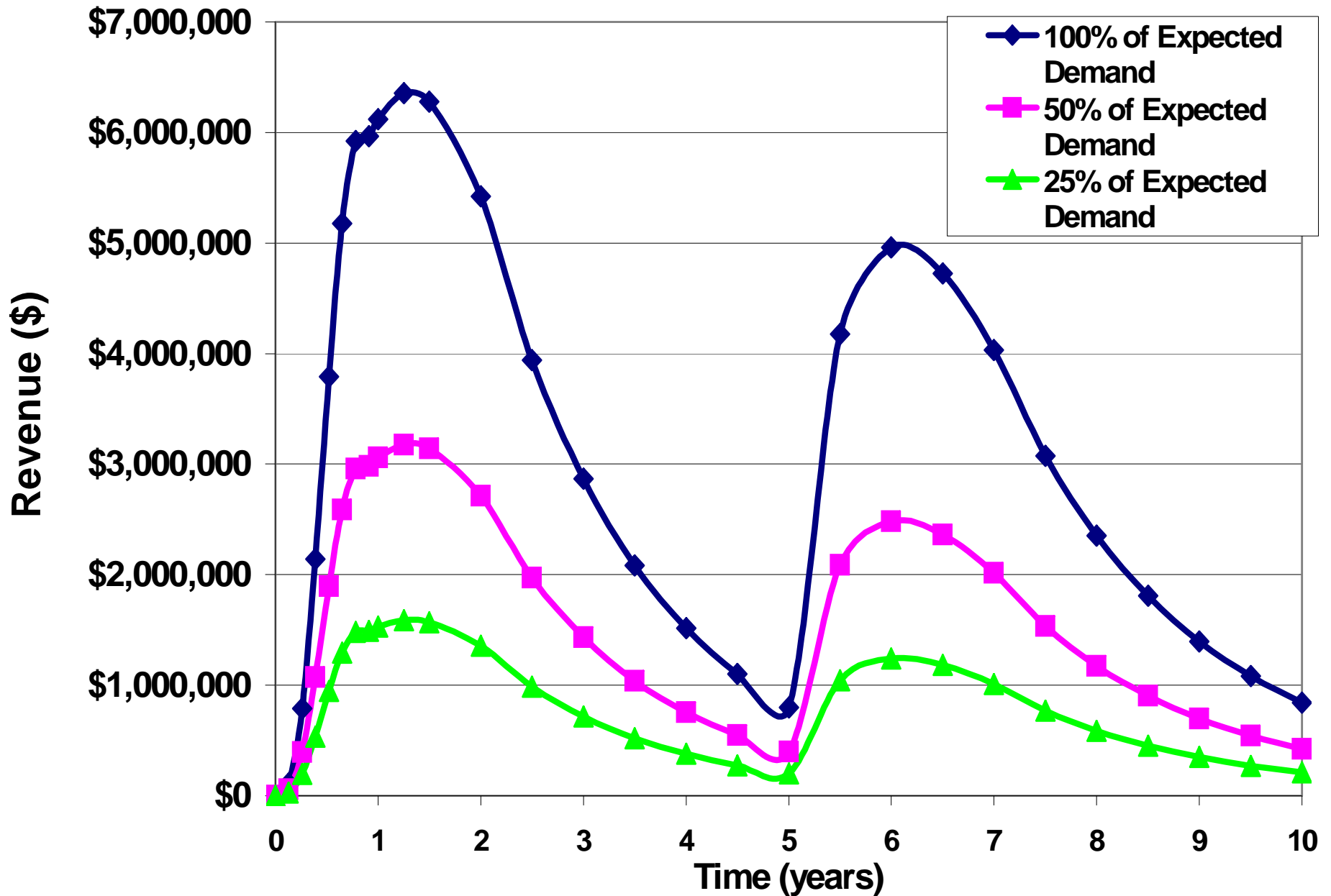
- Goal of this section is to predict profit if the scenario occurs that less consumers purchase the product.
- Consumer utility maximization could have predicted wrong.
- Copycats may enter market or oxygen prices may drop limiting market.

### Demand v Time (Varying Demand %)

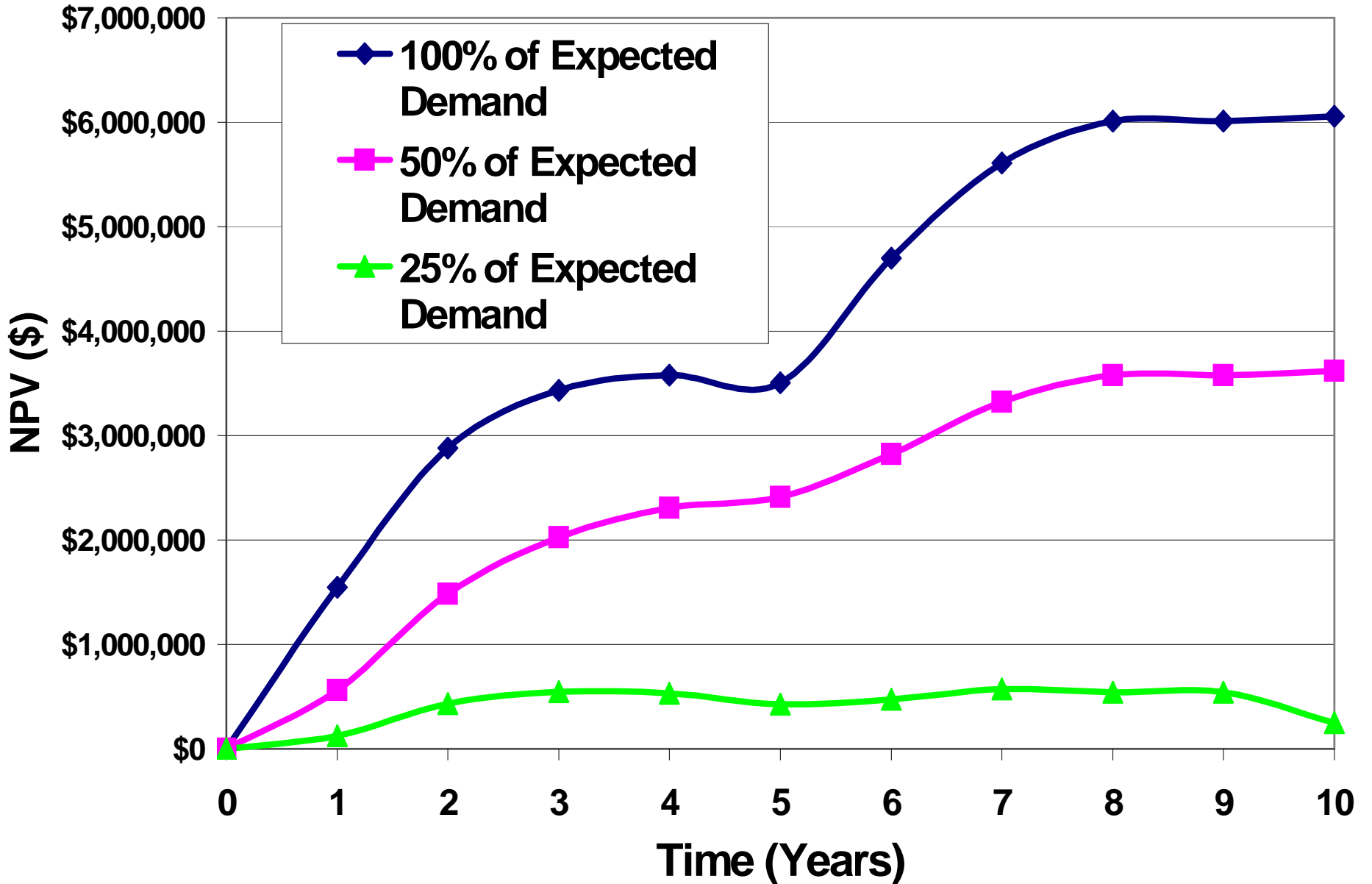




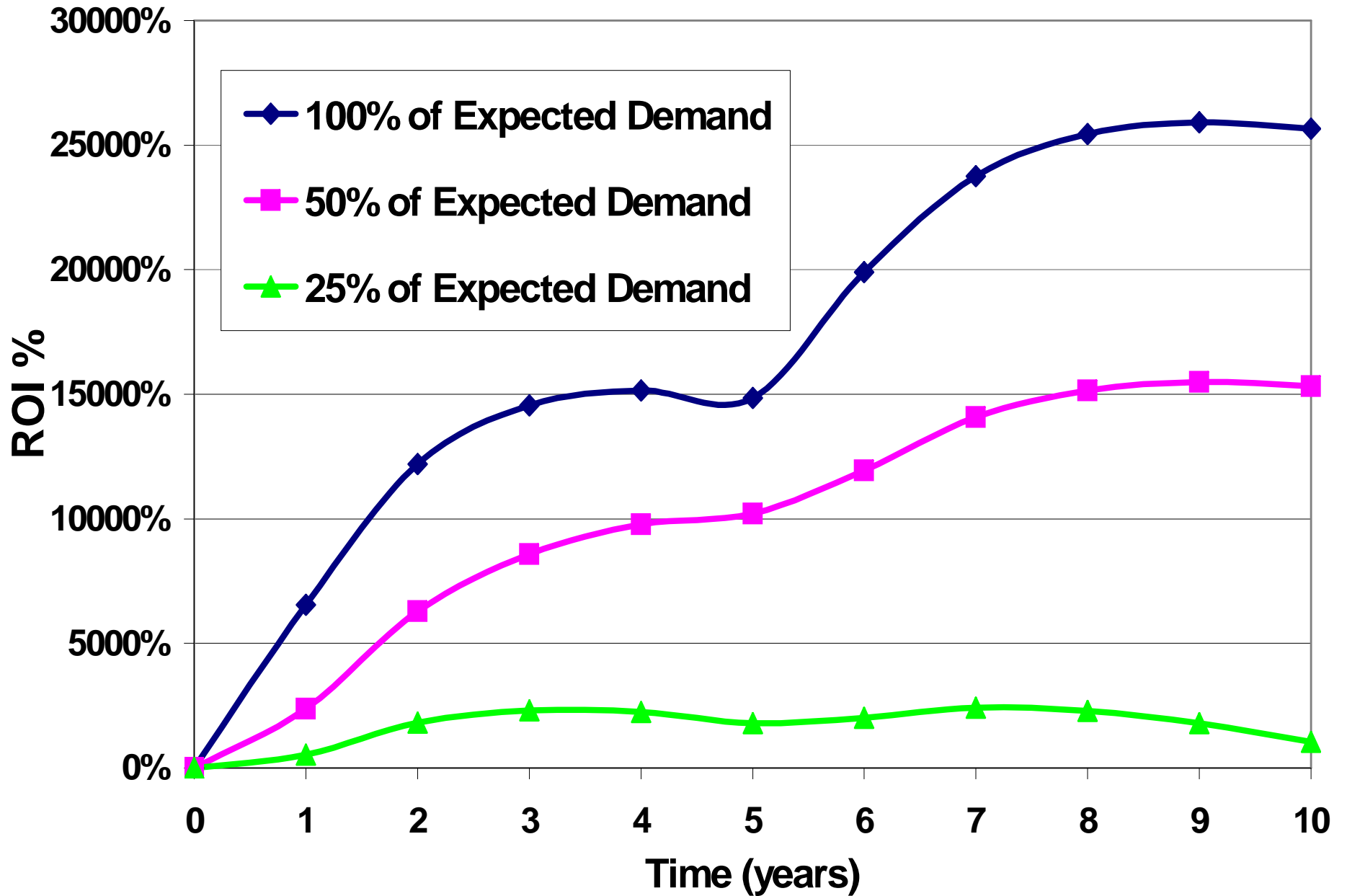
# Revenue v Time (Varying Demand)



## NPV v Time (Varying Demand)



# ROI v Time (Varying Demand)



# Conclusions

- The hospital project has been shown to be profitable even if demand is less than 75% than expected.
- NPV over 5 year span = \$2,800,000
- ROI over 1 year span = 5200%

# Future Work

- Research more into practical application of portable oxygen concentrators.
- Further studies on maximization of NPV, ROI, and hospital preferences.
- More in-depth analysis of risk and consumer/competitor reaction estimation.

# Business Model

## Preliminary Financial Analysis

	Concentrator	Liquid Oxygen
<b>Total Cost per 5 Year</b>	\$500,000	\$850,000
<b>Total Savings for 5 Years</b>	\$350,000	
<b>Average Savings per Year</b>	\$70,000	



# Final Conclusions

- It is now possible to deliver 99% oxygen to patients in a hospital, and to those who want to enjoy a life without the restriction of bulky liquid oxygen bottles.



# Final Conclusions

- This technology would change the lives of millions of patients and those needing oxygen around the world for years to come.





**Questions?**